

R. G. Prinn
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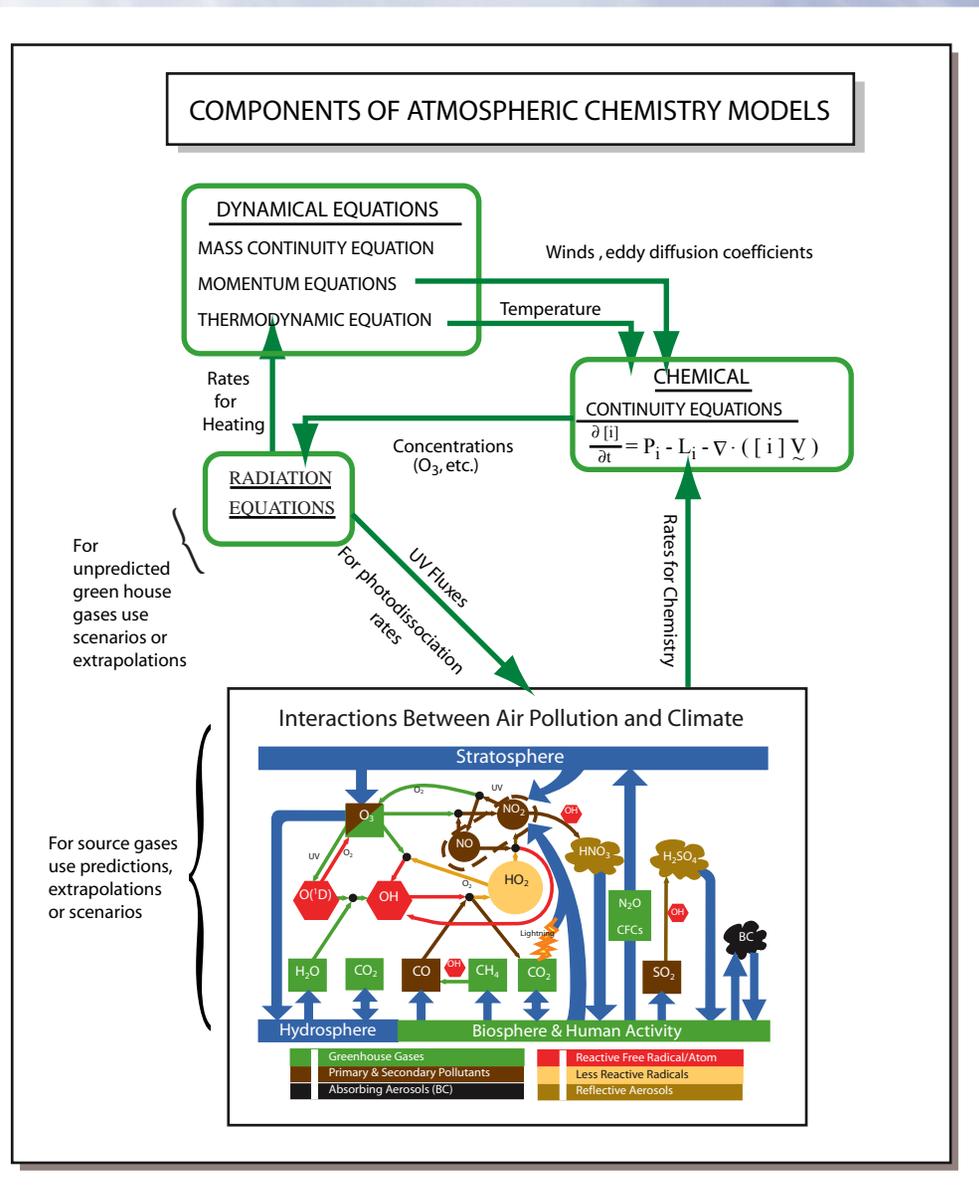


Figure by MIT OCW.

To solve the model equations, we divide the atmosphere into a finite number of boxes (grid cells).

Assume that each variable has the same value throughout the box.

Write a budget for each each box, defining the changes within the box, and the flows between the boxes.

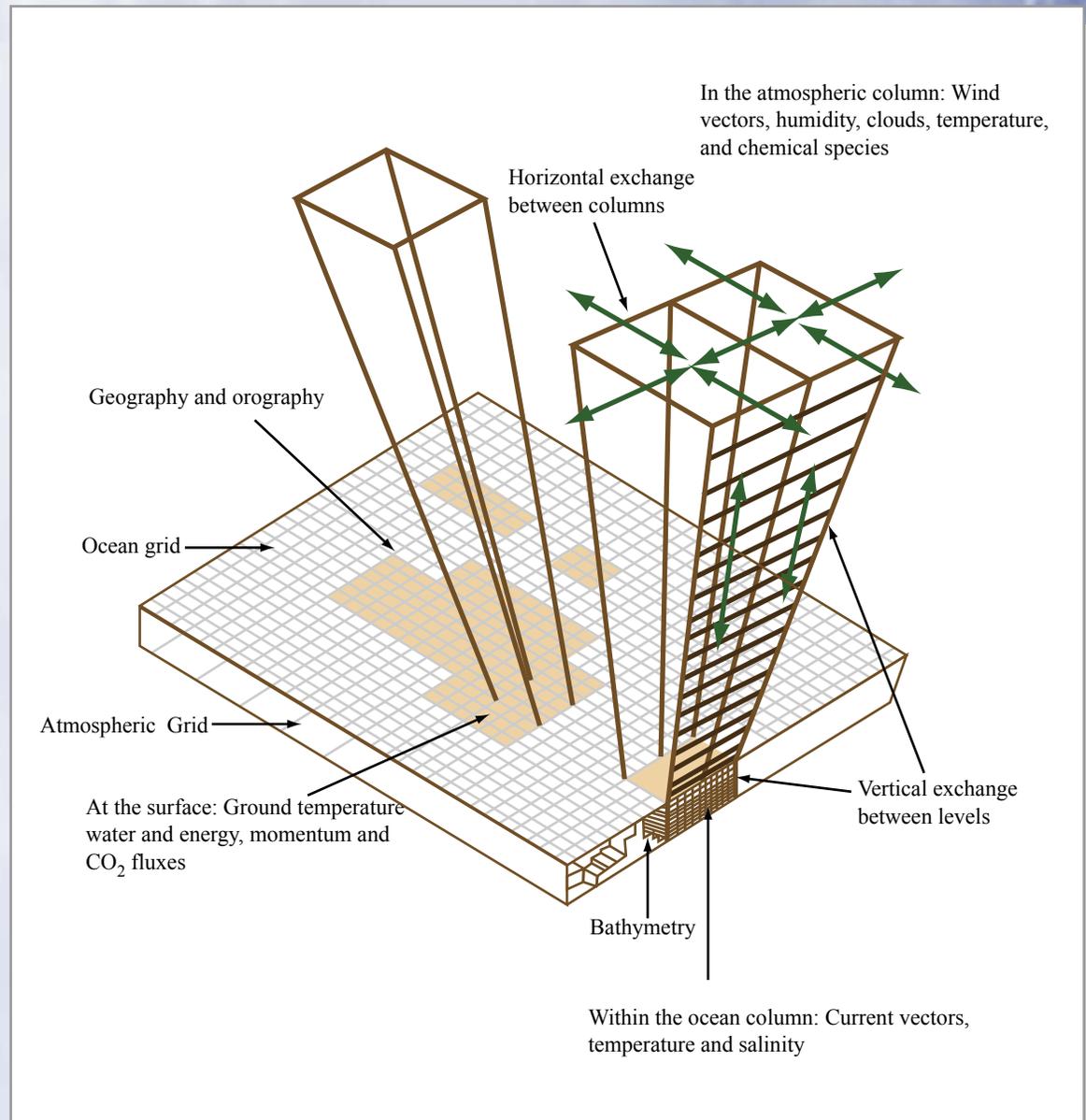


Figure by MIT OCW.

Physical picture:
(Eulerian)

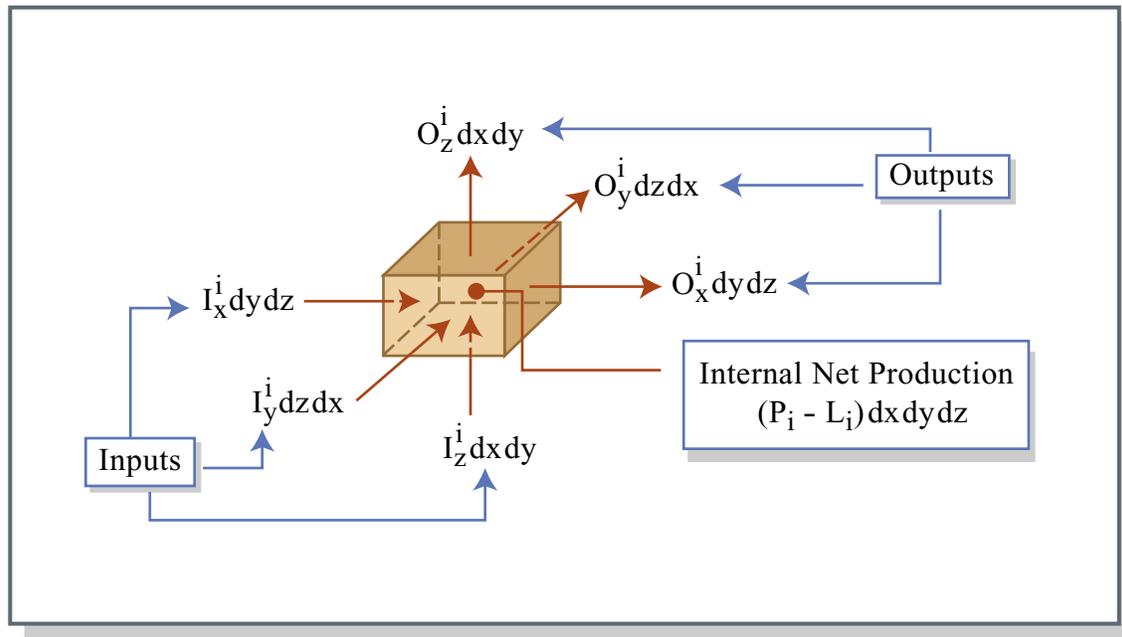


Figure by MIT OCW.

Notation:

$$\text{Inputs} = I_x^i dydz + I_y^i dzdx + I_z^i dxdy$$

$$\text{Outputs} = O_x^i dydz + O_y^i dzdx + O_z^i dxdy$$

$$= \left[I_x^i + \frac{\partial I_x^i}{\partial x} dx \right] dydz + \left[I_y^i + \frac{\partial I_y^i}{\partial y} dy \right] dzdx + \left[I_z^i + \frac{\partial I_z^i}{\partial z} dz \right] dxdy$$

$$I_x^i = [i]u, \quad I_y^i = [i]v, \quad I_z^i = [i]w \quad (\text{input fluxes})$$

$$u = \frac{dx}{dt}, \quad v = \frac{dy}{dt}, \quad w = \frac{dz}{dt} \quad (\text{wind velocities})$$

$P_i, L_i =$ rates of chemical production, loss

$[i] =$ concentration of i

Local rate of change of [i] given by:

$$\frac{\partial [i]}{\partial t} = \frac{\text{Inputs} - \text{Outputs} + \text{Internal net production}}{dxdydz}$$

$$= P_i - L_i - \frac{\partial}{\partial x}([i]u) - \frac{\partial}{\partial y}([i]v) - \frac{\partial}{\partial z}([i]w)$$

$$= P_i - L_i - \nabla \cdot ([i] \vec{V}) \quad (1)$$

Continuity equation for i

For total molecular concentration $[M]$, $P_M - L_M \approx 0$ so:

$$\frac{\partial [M]}{\partial t} = -\nabla \cdot ([M] \vec{V}) \quad (2)$$

Continuity equation for M

Defining mixing ratio = $[i]/[M] = X_i$:

$$\begin{aligned}
 \frac{\partial X_i}{\partial t} &= \frac{\partial}{\partial t} \left(\frac{[i]}{[M]} \right) = \frac{\frac{\partial [i]}{\partial t} [M] - \frac{\partial [M]}{\partial t} [i]}{[M]^2} \\
 &= \frac{\left(P_i - L_i - \nabla \cdot (X_i [M] \vec{V}) \right) [M] + \nabla \cdot ([M] \vec{V}) X_i [M]}{[M]^2} \quad \text{(Using equations (1) and (2))} \\
 &= \frac{\left(P_i - L_i - X_i \nabla \cdot ([M] \vec{V}) - [M] \vec{V} \cdot \nabla X_i \right) [M] + \nabla \cdot ([M] \vec{V}) X_i [M]}{[M]^2} \\
 &= \frac{\left(P_i - L_i - [M] \vec{V} \cdot \nabla X_i \right) [M]}{[M]^2} \\
 &= \frac{P_i - L_i}{[M]} - \vec{V} \cdot \nabla X_i \quad (3)
 \end{aligned}$$

Continuity Equation for i (mixing ratio form)

Theorem: If there is no gradient in the mixing ratio of i ($\nabla X_i = 0$) then there can be no local changes in i due to transport.

Rate of change of X_i traveling with the air given by (Lagrangian view):

$$\begin{aligned}
 (a) \quad \frac{dX_i}{dt} &= \frac{d}{dt} [X_i(x, y, z, t)] \\
 &= \frac{\partial X_i}{\partial x} \frac{dx}{dt} + \frac{\partial X_i}{\partial y} \frac{dy}{dt} + \frac{\partial X_i}{\partial z} \frac{dz}{dt} + \frac{\partial X_i}{\partial t} \quad \text{(chain rule)} \\
 &= \frac{\partial X_i}{\partial x} u + \frac{\partial X_i}{\partial y} v + \frac{\partial X_i}{\partial z} w + \frac{\partial X_i}{\partial t} \\
 &= \vec{V} \cdot \nabla X_i + \frac{P_i - L_i}{[M]} - \vec{V} \cdot \nabla X_i \quad \text{(using equation (3))} \\
 &= \frac{P_i - L_i}{[M]} \quad (4)
 \end{aligned}$$

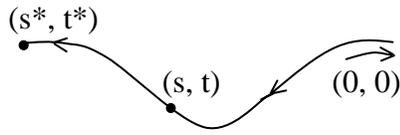
Theorem: If there is no “net chemical production” ($P_i - L_i = 0$), then the mixing ratio of i is conserved moving with the air.

(b)

$$X_{it^*} = X_{i0} + \int_0^{s^*} \frac{dX_i}{dt} \frac{dt}{ds} ds$$

$$= X_{i0} + \int_0^{s^*} \frac{P_{is} - L_{is}}{[M]} u_s ds$$

(using equation (4)) (5)



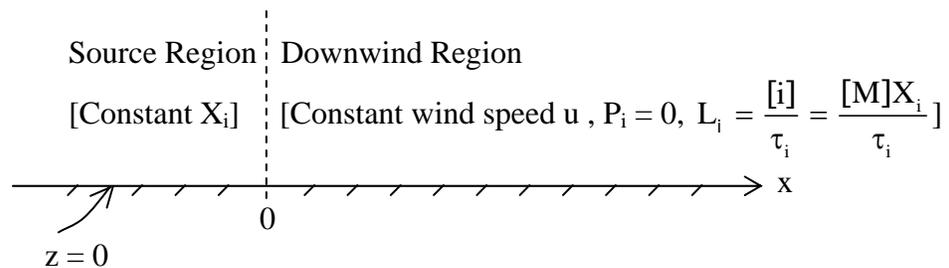
Theorem: The change in mixing ratio in an air mass from its initial value is a line integral of the “net chemical production” over the trajectory of the air mass.

A steady state exists when the local rate of change is zero:

$$\left. \begin{aligned} \frac{\partial [i]}{\partial t} = 0 & \quad \text{i.e. } P_i - L_i = \nabla \cdot ([i] \vec{V}) \\ \frac{\partial [M]}{\partial t} = 0 & \quad \text{i.e. } \nabla \cdot ([M] \vec{V}) = 0 \end{aligned} \right\} (6)$$

$$\frac{\partial X_i}{\partial t} = 0 \quad \text{i.e. } \frac{P_i - L_i}{[M]} = \vec{V} \cdot \nabla X_i \quad (7)$$

One-Dimensional (Horizontal) Model



Equation (7) with $v = w = 0$ gives:

$$\begin{aligned} P_i - L_i &= 0 - [M] \frac{X_i}{\tau_i} \\ &= [M] u \frac{dX_i}{dx} \\ \text{i.e. } \frac{d \ln X_i}{dx} &= -\frac{1}{u \tau_i} \end{aligned}$$

$$\text{i.e. } X_i(x) = X_i(0) \exp\left(-\frac{x}{u \tau_i}\right) \quad (8)$$

[chemical (e-folding) distance, $h = u\tau_i$]

[advection time = x/u]

i.e.

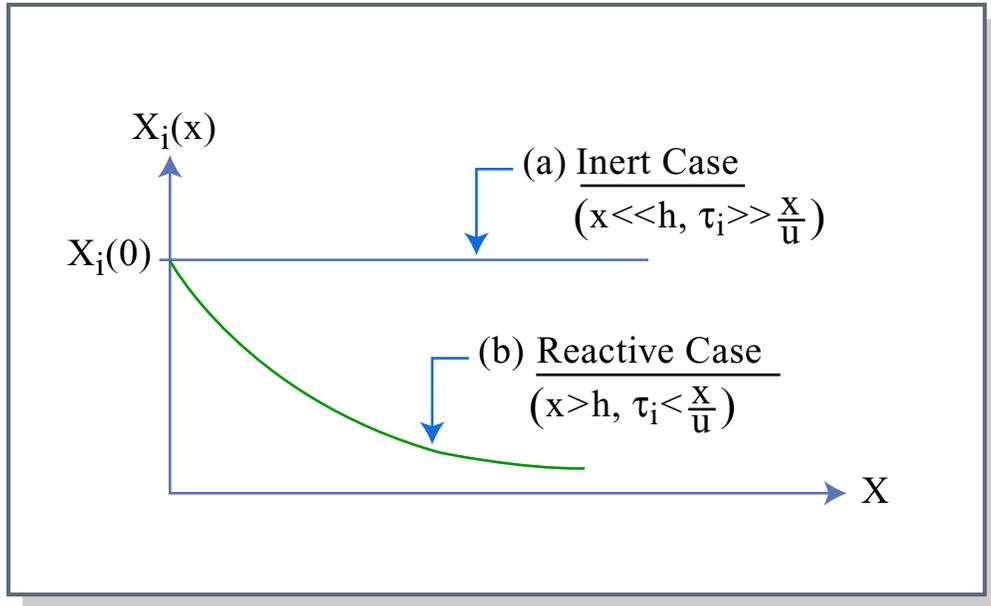


Figure by MIT OCW.