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8.21 The Physics of Energy  
Fall 2009

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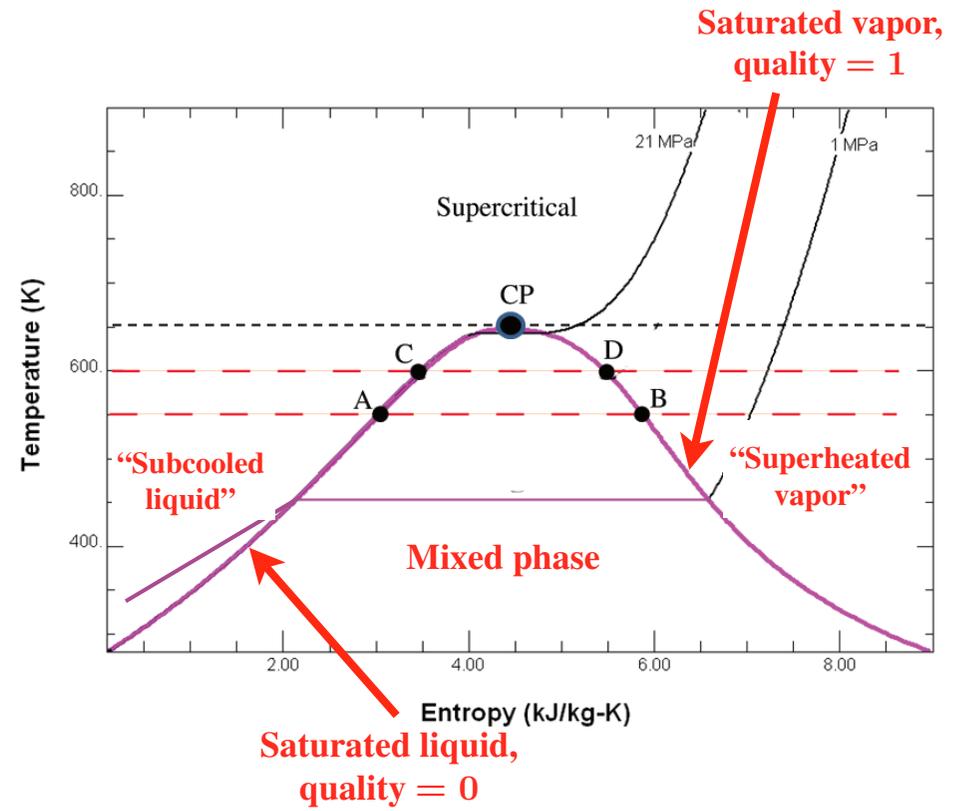
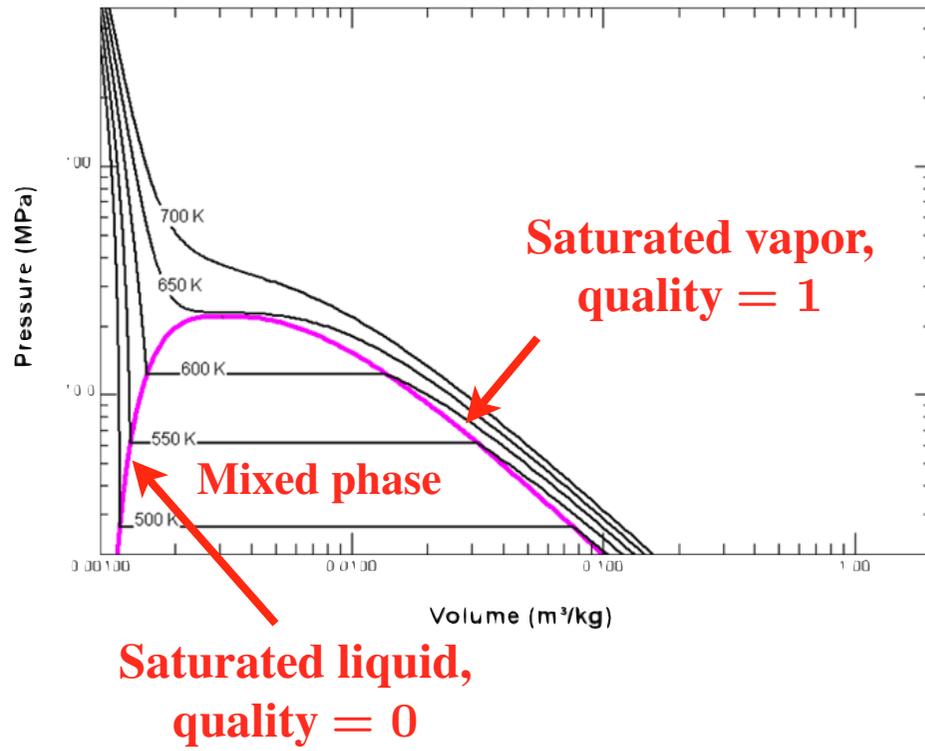
## 8.21 Lecture 12

# Phase Change Energy Conversion II

October 5, 2009

- Use what we learned @ change of phase on Wednesday to build workhorse devices today.
- The vapor compression cycle: heat pumps, refrigeration, air conditioners
- The Rankine steam cycle and steam turbines
- Some implementations of the Rankine cycle
- Marks end of Part I of the course on the “Uses of Energy”. Wednesday begins Part II on “Energy Sources”

# Reminder: Thermodynamics of phase change:

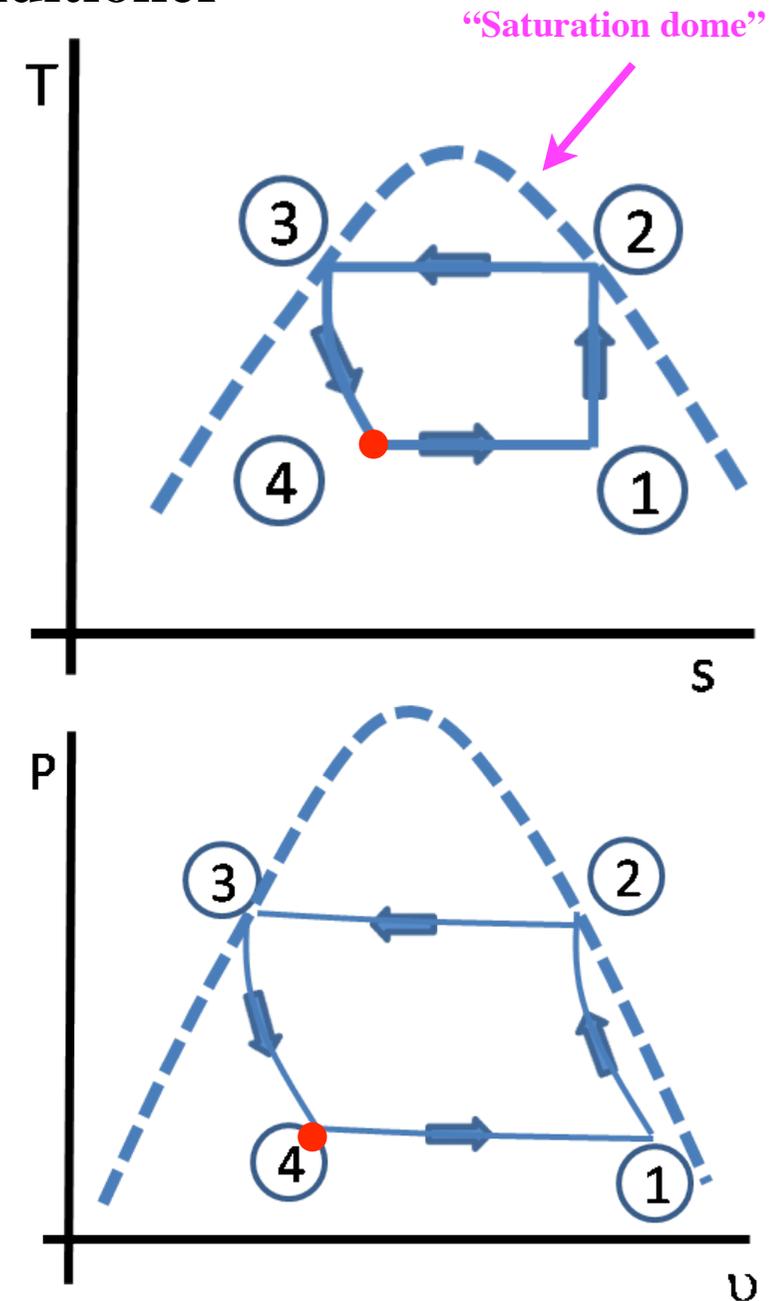


# Let's build a vapor-compression cycle air conditioner

So now lets combine cycle analysis with our new knowledge of the thermodynamics of a fluid that can change phase

## Environments and Cycle Steps

- ★ **First step:** From liquid rich mixed phase to vapor rich mixed phase at low temperature and pressure,  $T_L$  and  $P_L$ . **EVAPORATOR**
- ★ **Second step:** Compression from vapor rich mixed phase at  $(T_L, P_L)$  to pure vapor at  $(T_H, P_H)$ . **COMPRESSOR**
- ★ **Third step:** From pure vapor at  $(T_H, P_H)$  to pure liquid still at high temperature and pressure,  $(T_H, P_H)$ . **CONDENSER**
- ★ **Fourth step:** Free expansion from  $(T_H, P_H)$  to  $(T_L, P_L)$ . **THROTTLE**



## Step [12] iso-entropic (adiabatic) compression

- Enter cycle at ①  
 $T_L$  and  $P_L$  in mixed phase, mostly vapor (high quality).
- Compress keeping heat exchange with surroundings to a minimum
- Do work on fluid, but allow no heat transfer  $\Rightarrow$  enthalpy of fluid increases:

**Must increase quality** (change liquid to vapor)

- Result: hot, high pressure, saturated vapor at ②.

★  $W_{12}$  done **on** fluid

★  $Q_{12} = 0$

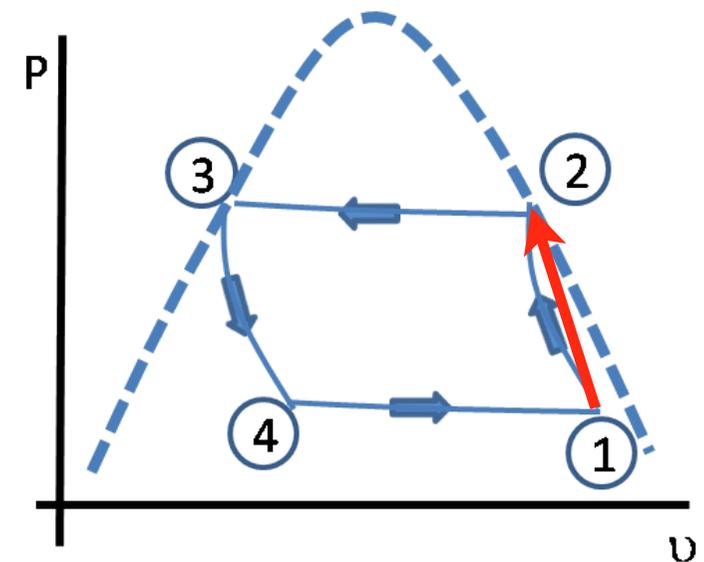
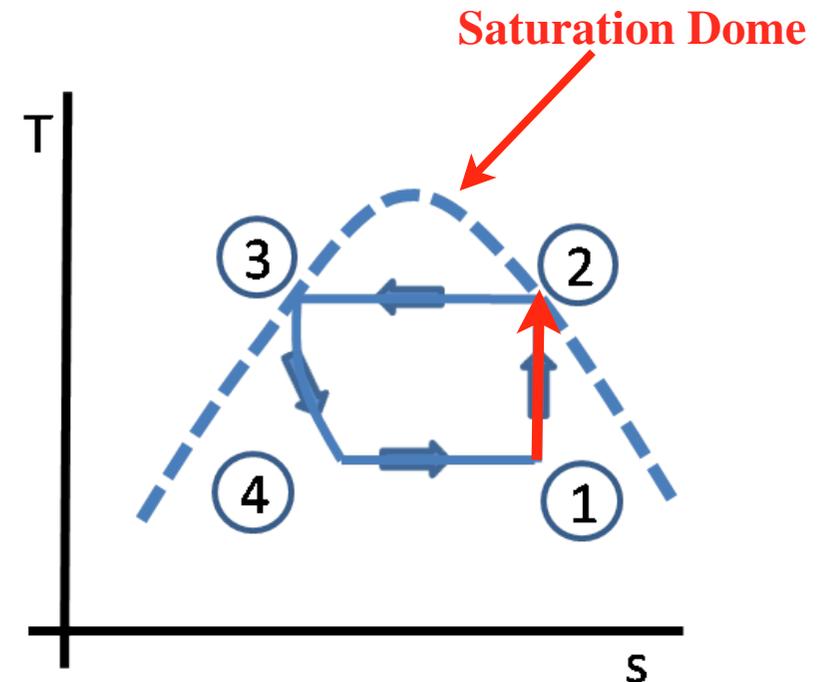
- Compressor is placed in warm zone (eg. outside refrigerator or home living space)

$$dH = dU + pdV + Vdp$$

$$dQ = dU + pdV = 0 \quad \text{So,}$$

$$dH = Vdp$$

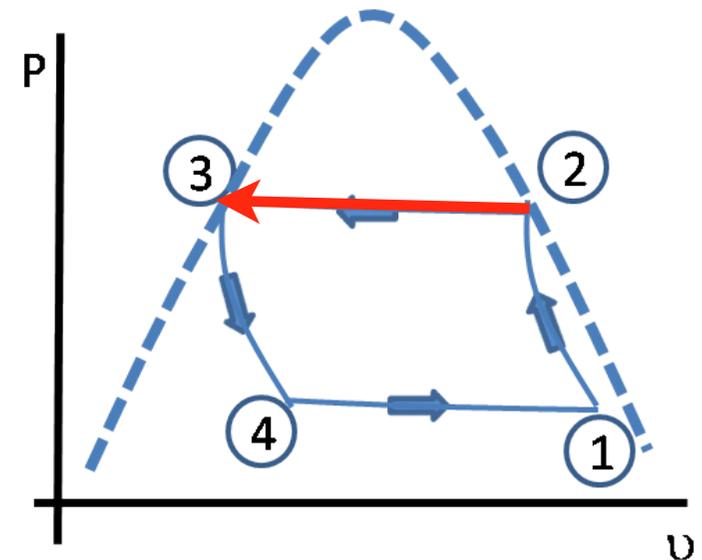
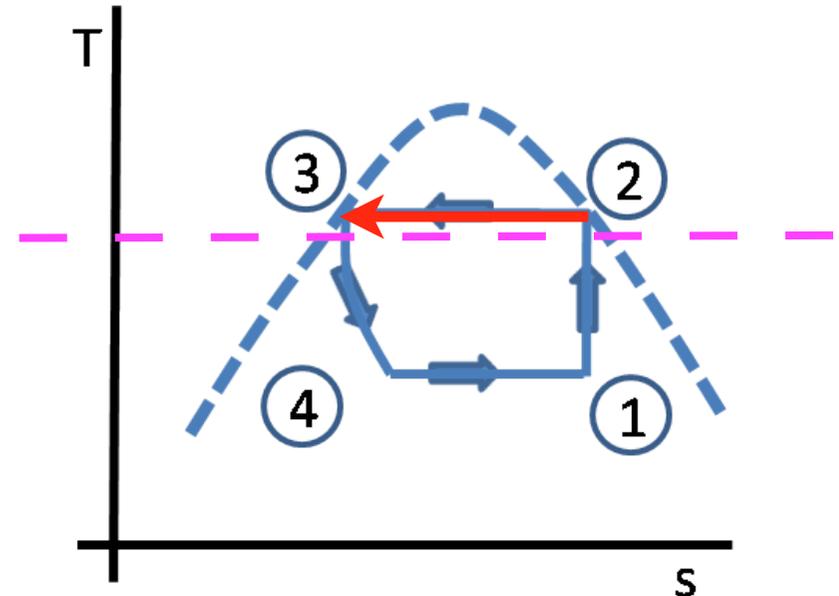
$$\Delta H = \int_{P_L}^{P_H} dp V > 0$$



## Step [23] isothermal condensation

- Start at ②  
Saturated vapor at  $T_H$  and  $P_H$
- Allow vapor to condense by ejecting heat to high temperature environment.
- Enthalpy (heat) escapes and saturated vapor condenses to saturated liquid.
- Superficially similar to isothermal compression of Carnot cycle, but here no work is done.
- Result: Hot, high pressure saturated liquid ③.
  - ★  $W_{23} = 0$
  - ★  $Q_{23} = Q_H$
- Condenser is placed in warm zone (eg. outside refrigerator or home living space)

$T_H$  exceeds  
temperature of  
hot environment



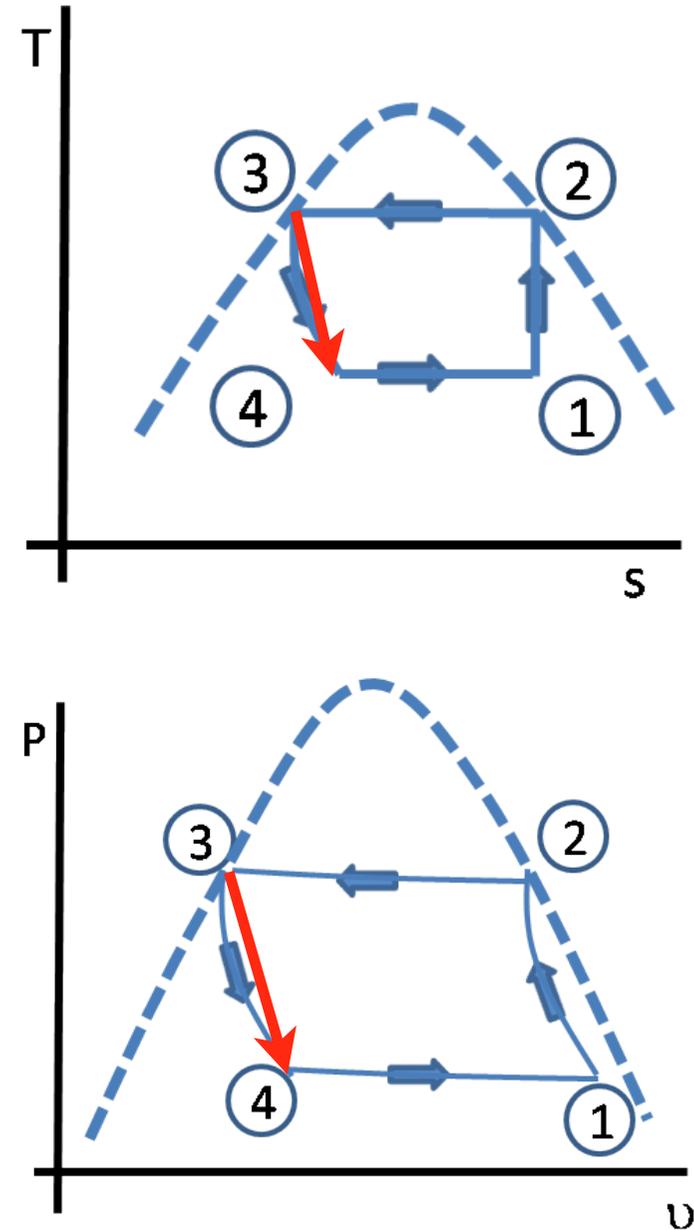
## Novel!

### Step [34] iso-enthalpic expansion

- Start at ③ Saturated liquid at  $T_H$  and  $P_H$
- Allow liquid to expand through a *throttle* into a low pressure region
- **Entropy grows** and **temperature drops**.
- Look at  $TS$ -plane:  $(T \downarrow) \ \& \ (S \uparrow) \Rightarrow$  **liquid  $\rightarrow$  vapor**
- Result: Cold, low pressure mixed phase, of low quality — liquid rich, at point ④.

★  $\Delta H_{34} = 0$

★  $Q_{34} = 0$



## Expansion of saturated liquid through a nozzle

- ★ Pressure decreases and volume increases.
- ★ Starting point *I* at saturation

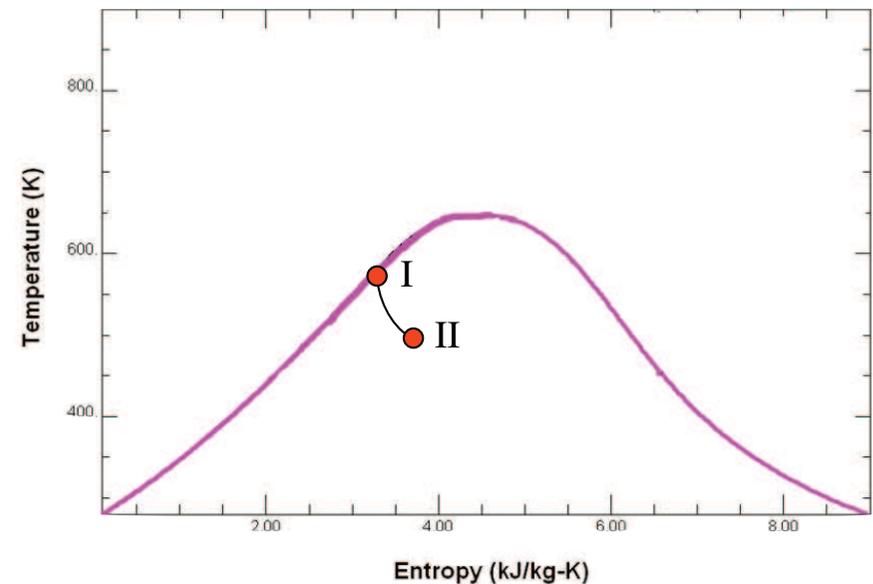
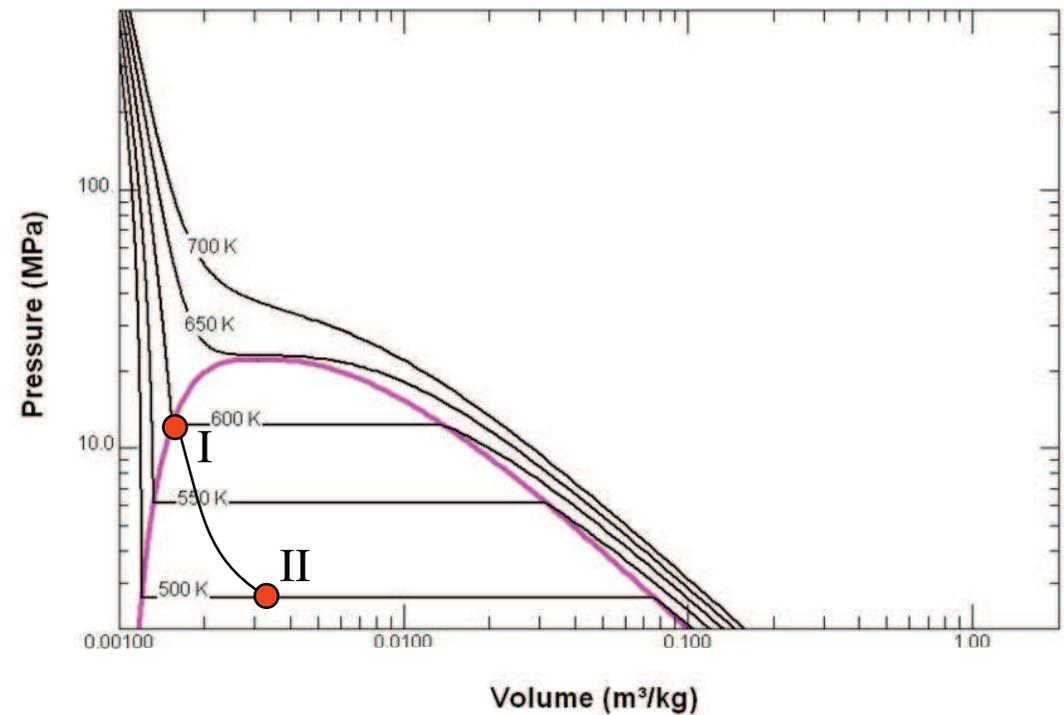
Moves into mixed phase at *II*

- ★ Trace in *ST* diagram

Remember  $\Delta S > 0$ .

Temperature must decrease

Quality (fraction of vapor) must increase



## Step [41] isothermal evaporation

- Start at ④
- Liquid rich mixed phase at  $T_L$  and  $P_L$
- Allow liquid to evaporate, extracting heat from the low temperature environment.
  - ★  $W_{41} = 0$
  - ★  $Q_{41} = Q_L$
- Result: Cold, low pressure mixed phase, of now of high quality — vapor rich, at point ①.

$T_L$  is below temperature of hot environment

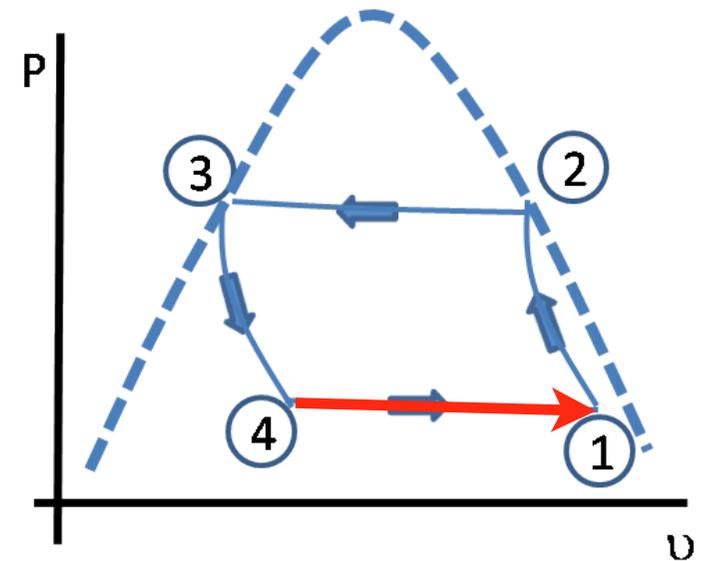
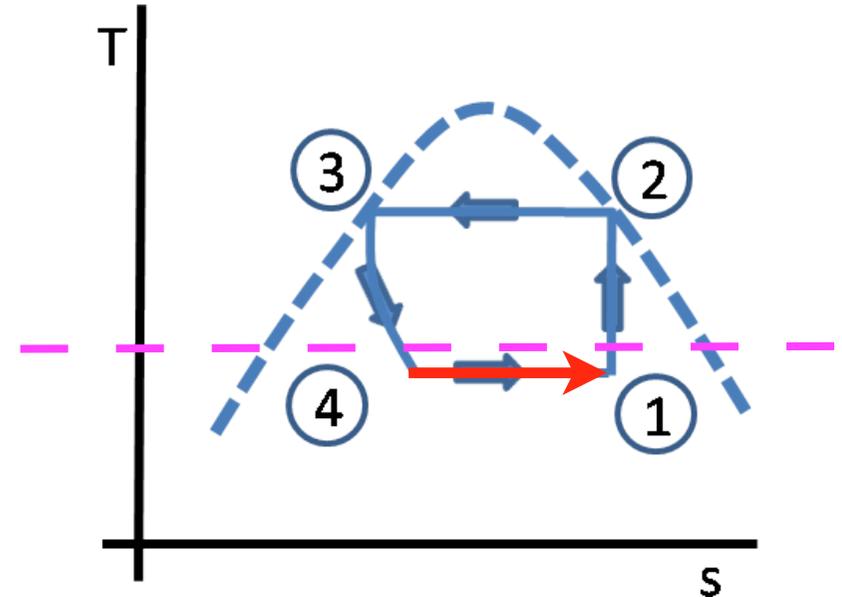
## Summarizing energy flow

★ Work done only in compressor:  $W_{[12]}$

★ Heat removed from low  $T$ :  $Q_{[41]}$

Heat ejected to high  $T$ :  $Q_{[23]}$

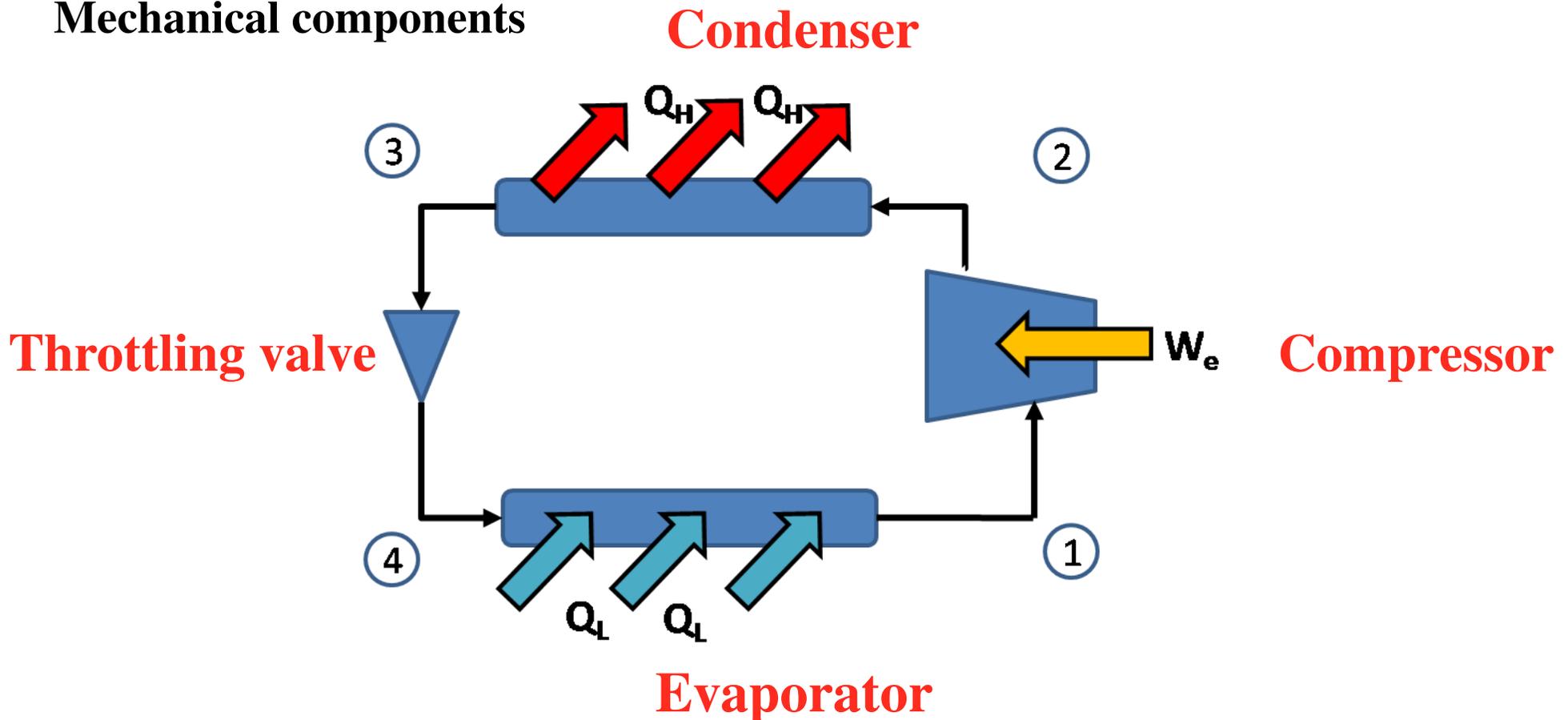
$$\text{CoP}_{\text{air conditioner}} = \frac{Q_{[41]}}{W_{[12]}} \quad \text{CoP}_{\text{heat pump}} = \frac{Q_{[23]}}{W_{[12]}}$$



## Entropy

- All steps were reversible, except for small irreversibility during throttling, so coefficient of performance cannot quite reach Carnot limit

## Mechanical components



## A scroll compressor

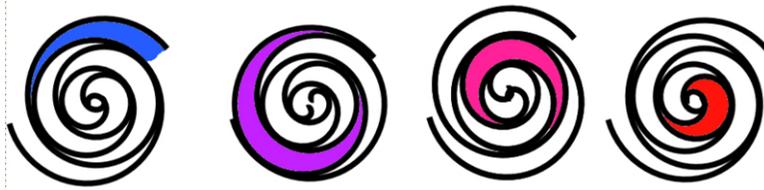


Image from public domain.

## A screw-type compressor



From [http://commons.wikimedia.org/wiki/File:Lysholm\\_screw\\_rotors.jpg](http://commons.wikimedia.org/wiki/File:Lysholm_screw_rotors.jpg)

## Same principle as throttle

Hair spray image removed  
due to copyright restrictions.

Please see:

<http://www.grainprocessing.com/images/Hair%20Spray.jpg>

## Condenser for refrigerator

Condenser image removed  
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Please see:

[http://img.alibaba.com/photo/11160583/  
Condenser\\_For\\_Refrigerator\\_Water\\_Coolers.jpg](http://img.alibaba.com/photo/11160583/Condenser_For_Refrigerator_Water_Coolers.jpg)

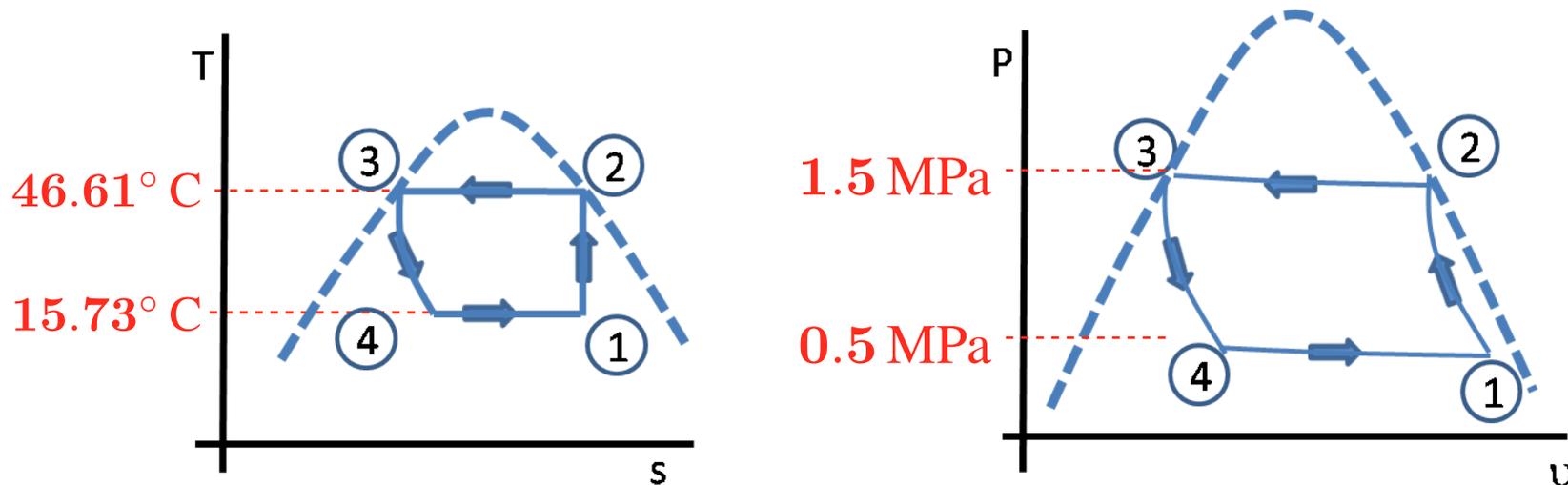
## Evaporator for air conditioner

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due to copyright restrictions.

Please see:

[http://img.diytrade.com/cding/  
520742/3323685/0/1173261417/A\\_C\\_Evaporator.jpg](http://img.diytrade.com/cding/520742/3323685/0/1173261417/A_C_Evaporator.jpg)

# A quasi-realistic implementation of The Ideal Vapor Compression Cycle



Stage	T (C)	P (MPa)	energy ( $\frac{kJ}{g}$ )	enthalpy ( $\frac{kJ}{kg}$ )	entropy ( $\frac{kJ}{kgK}$ )	quality
1	15.73	0.5	218.28	238.5	0.83968	0.9830
2	46.61	1.2	236.17	256.23	0.83968	1
3	46.61	1.2	99.065	100.14	0.35107	0
4	15.73	0.5	92.425	100.14	0.3607	0.2390

## Performance

★  $\Delta W_{[12]} = 17.73 \text{ kJ/kg}$

★  $\Delta Q_{[41]} = 138.13 \text{ kJ/kg}$

★  $CoP = 138.13/17.73 = 7.79$

★ 5 tons cooling (?) = 17.5 kW

★  $\dot{m} = .126 \text{ kg/sec}$  and  $P_{electric} = 2.25 \text{ kW}$

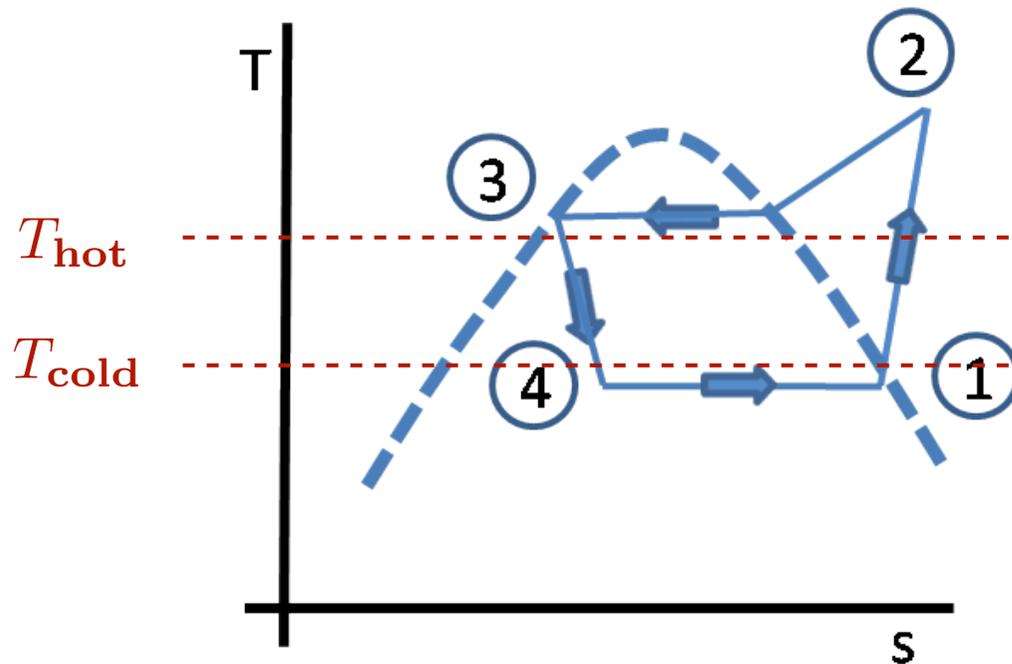
Only the beginning of an engineering design iteration...

## A more realistic vapor compression cycle

- ★ Many small items: frictional losses in pipes, thermal losses in compressor and throttle.
- ★ Temperatures of hot and cold spaces must exceed set points of cycle in order to get efficient heat transfer
- ★ But one significant design issue

Compressor cannot handle mixed phase without mechanical damage

- ★ Modify cycle so compressor works entirely in “superheated” vapor phase.



- Why this now?
- Thermodynamics of heat extraction
- Phase change in pure substances
- The vapor compression cycle: heat pumps, refrigeration, air conditioners
- The Rankine steam cycle and steam turbines
- Some implementations of the Rankine cycle

# Steam Engines! Parallels history of Industrial Revolution

At the heart of energy  
consumption revolution of  
1800's

- ★ Heron of Alexandria circa 1st century AD
- ★ Thomas Newcomen (British 17th c), James Watt (British 18th c), developed reciprocating (pistons and cylinders, etc.) steam engines.
- ★ Charles Parsons (also British, 19th-20th c), developed steam turbine, using *Rankine Cycle*, which revolutionized power generation.

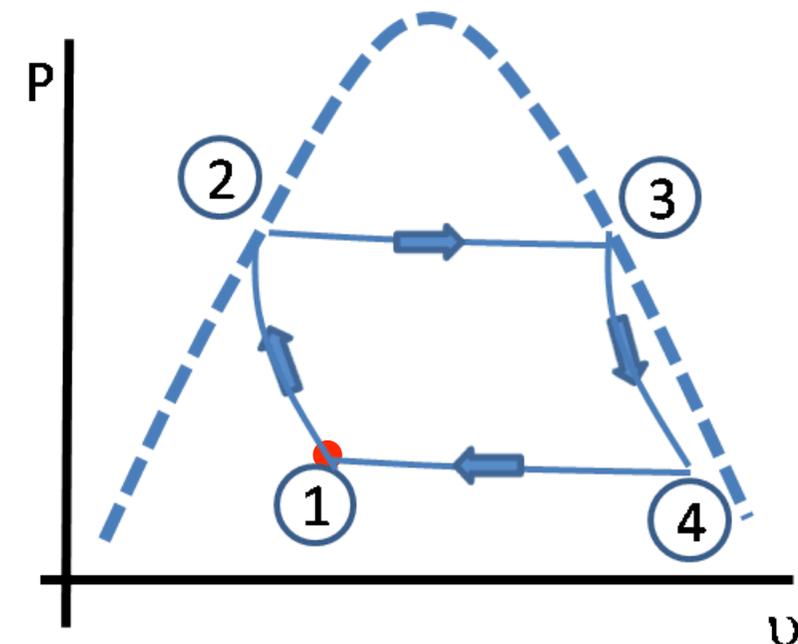
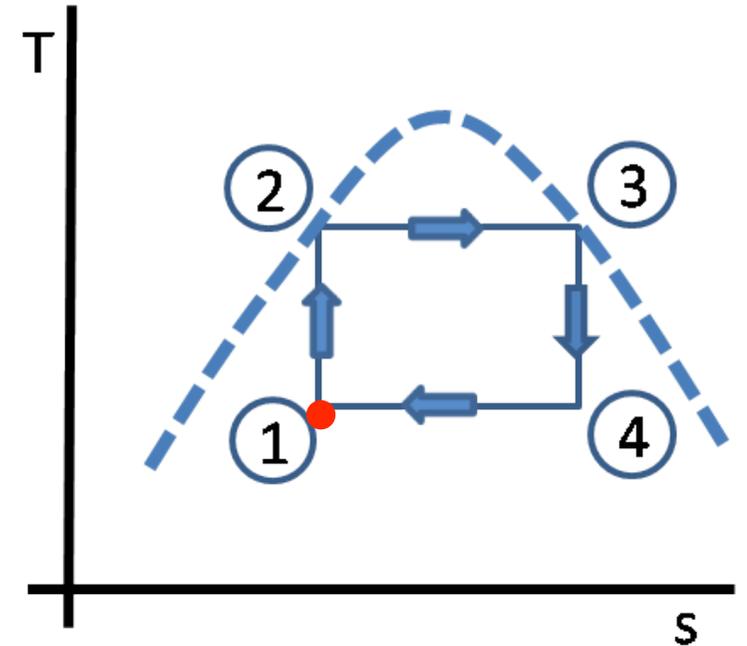
Steam engine images removed  
due to copyright restrictions.

## Rankine Cycle:

Conceptually, vapor compression cooling cycle run backward

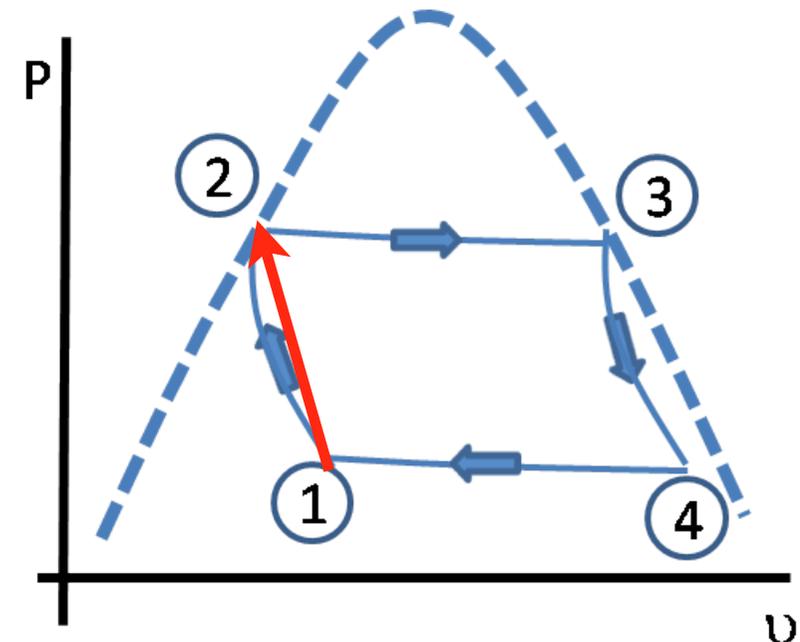
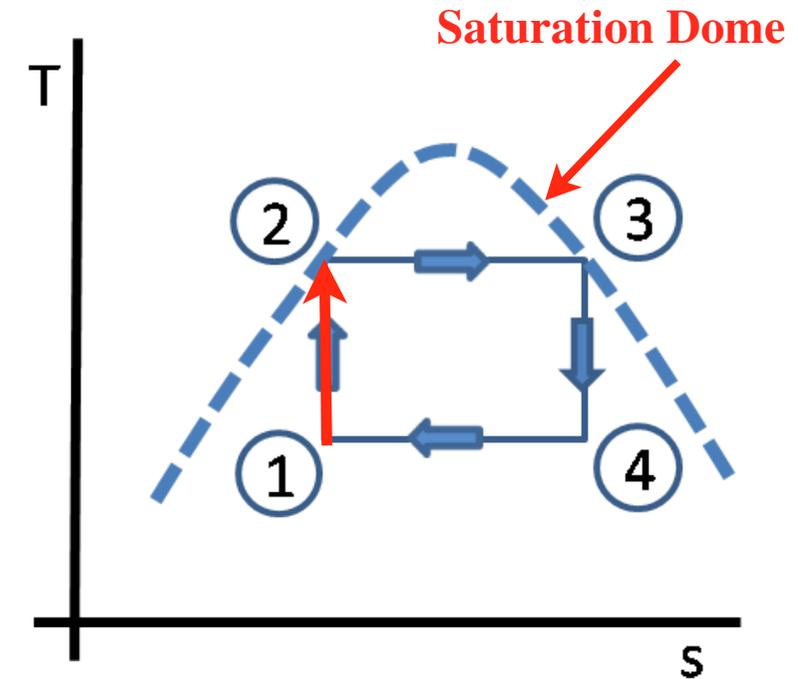
### Environments and Cycle Steps

- ★ **First step:** Mixed fluid of low quality (exhausted) at  $(T_L, P_L)$  is compressed to pure liquid (zero quality) at  $(T_H, P_H)$ . **PUMP**
- ★ **Second step:** Pure liquid at  $(T_H, P_H)$  absorbs heat and converts to pure vapor at  $(T_H, P_H)$ . **BOILER**
- ★ **Third step:** Pure vapor at  $(T_H, P_H)$  expands adiabatically (doing work) to mixed phase of high quality at  $(T_L, P_L)$ . **TURBINE**
- ★ **Fourth step:** Mixed phase of high quality at  $(T_L, P_L)$  expels heat and converts to mixed phase of low quality at  $(T_L, P_L)$ . **CONDENSER**



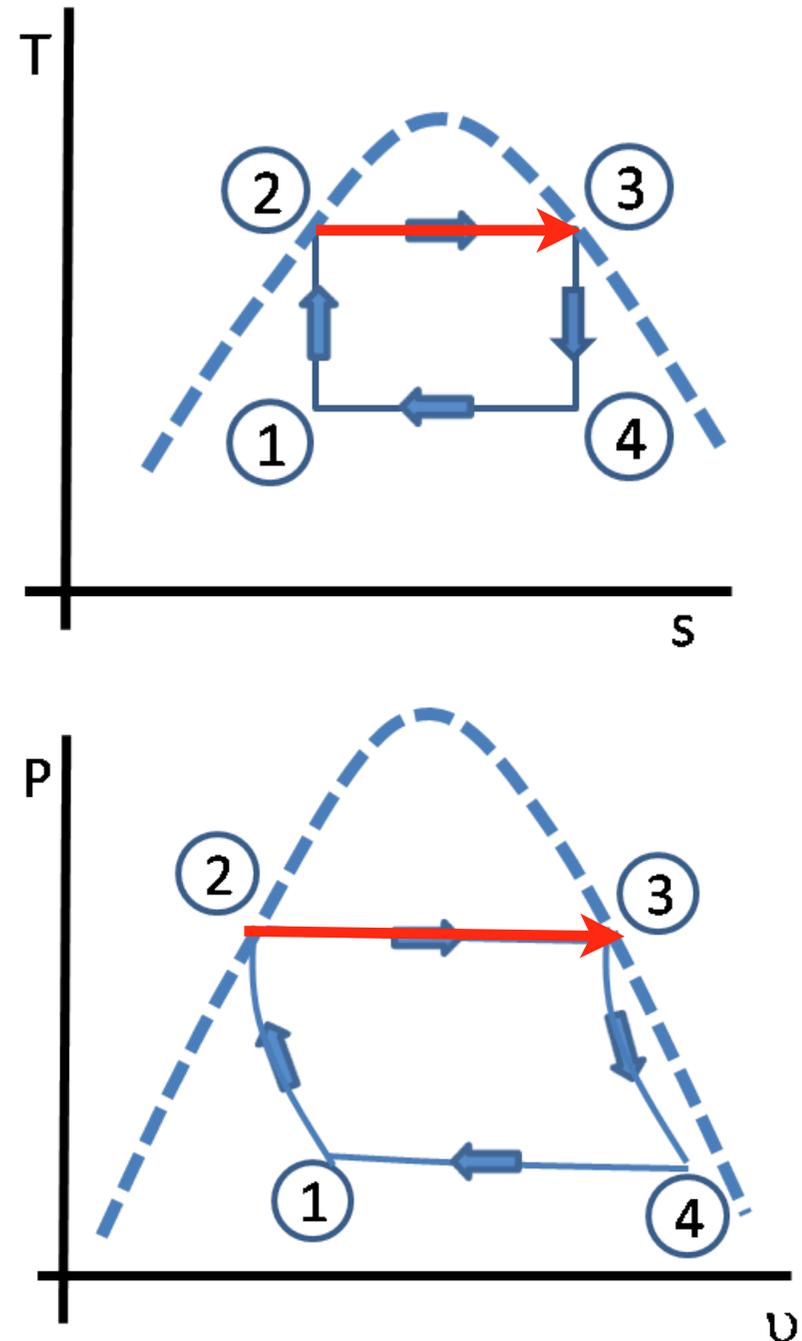
## Step [12] iso-entropic (adiabatic) compression

- Enter cycle at ①
  - $T_L$  and  $P_L$  in mixed phase, mostly water (low quality).
- Compress keeping heat exchange with surroundings to a minimum
- Do work on fluid, but allow no heat transfer  $\Rightarrow$  enthalpy of fluid increases.
- Result: hot, high pressure, saturated liquid at ②.
  - ★  $W_{12} = W_{\text{pump}}$  done **on** fluid
  - ★  $Q_{12} = 0$
- **Pump**



## Step [23] isothermal vaporization (boiling)

- Start at ②
- Saturated liquid at  $T_H$  and  $P_H$
- Add heat in combustion chamber/boiler
- Enthalpy (heat) converts liquid water to steam at constant temperature and pressure
- Superficially similar to isothermal expansion of Carnot cycle, but here no work is done.
- Result: Hot, high pressure saturated vapor ③.
  - ★  $W_{23} = 0$
  - ★  $Q_{23} = Q_H$



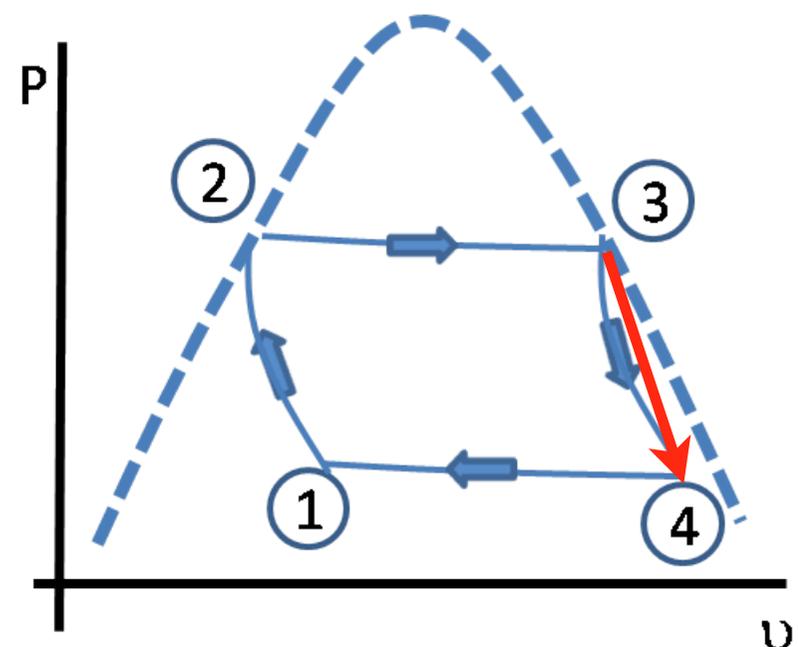
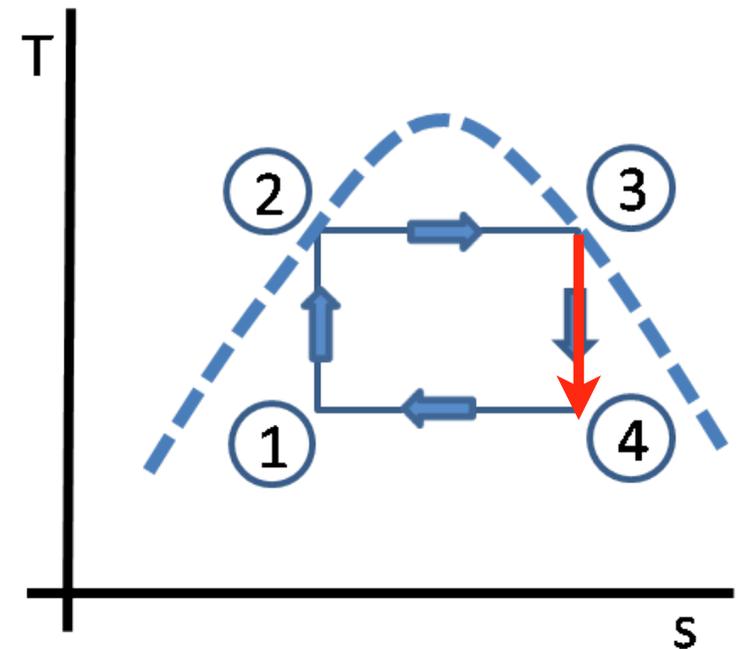
## Novel!

### Step [34] isentropic expansion through turbine

- Start at ③ High energy density vapor at  $T_H$  and  $P_H$
- Force steam to do work against blades of a turbine
- Minimize heat exchange,  $\Delta S \approx 0$
- **Temperature, pressure and quality all drop**
- **Result: Cooler, low pressure mixed phase, though still of high quality — vapor rich, at point ④.**

★  $W_{34} = W_{\text{useful}}$

★  $Q_{34} = 0$



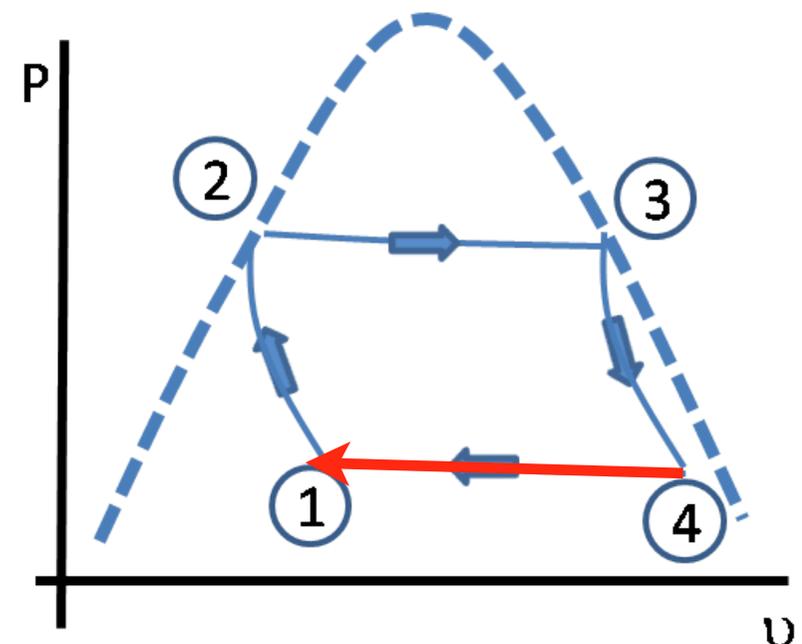
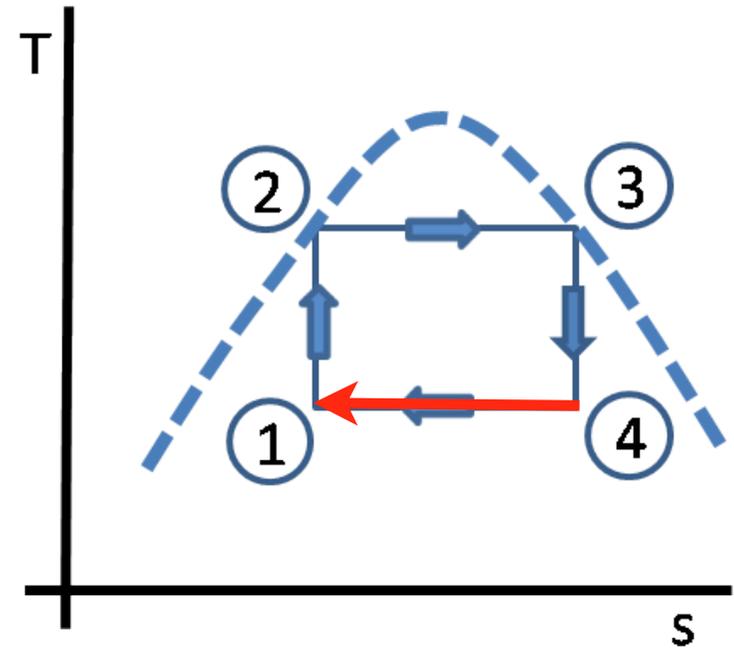
## Step [41] isothermal condensation

- Start at ④
- Vapor rich mixed phase at  $T_L$  and  $P_L$
- Allow steam to condense, expelling heat to environment.
  - ★  $W_{41} = 0$
  - ★  $Q_{41} = Q_L$
- Result: Cold, low pressure mixed phase, of now of low quality — liquid water rich, at point ①.

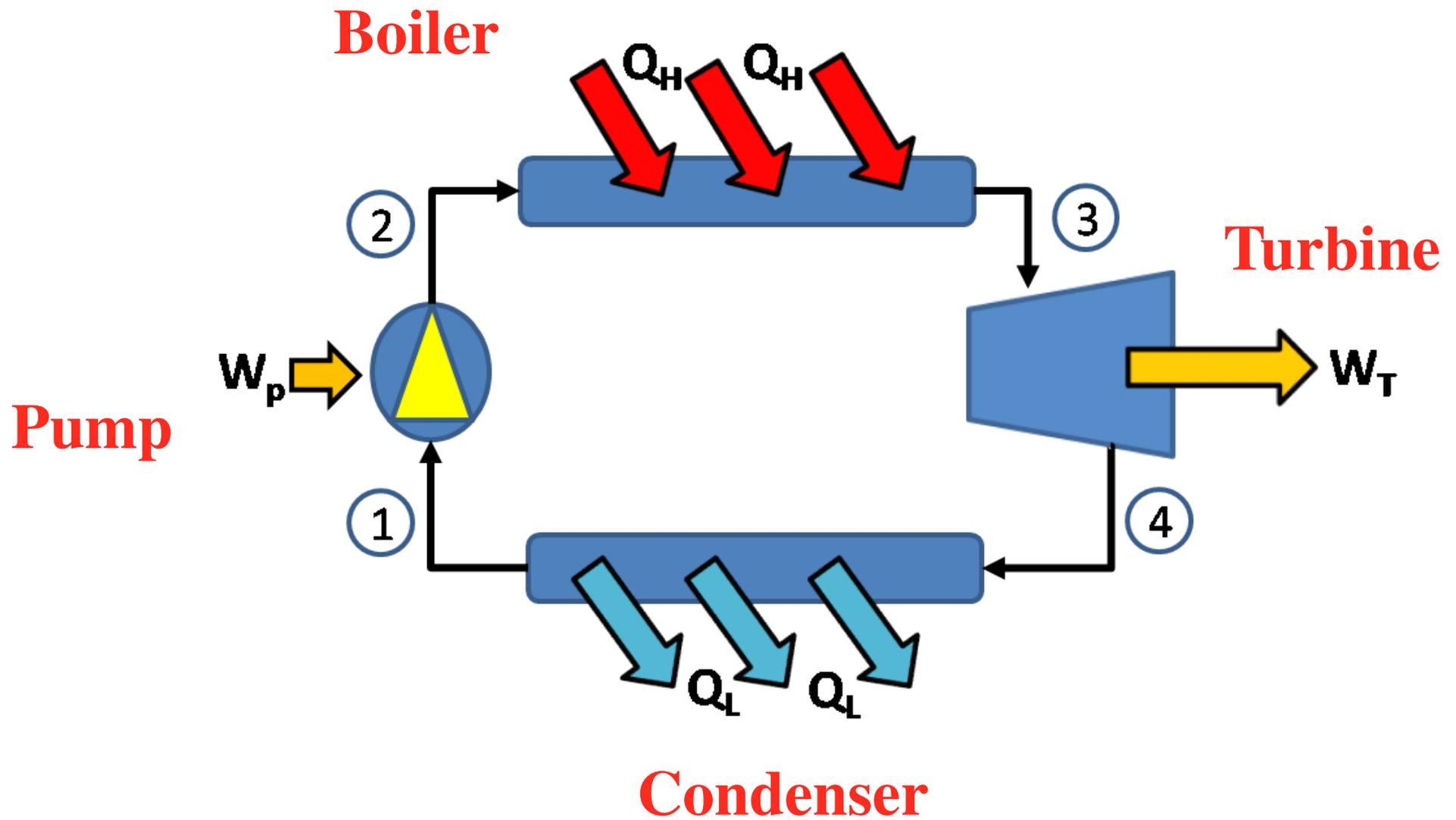
## Summarizing energy flow

- ★ Net work:  $W_{[34]} - W_{[12]}$
- Turbine – pump
- ★ Heat take from high  $T$ :  $Q_{[23]}$
- Heat ejected to low  $T$ :  $Q_{[41]}$

$$\text{CoP} = \frac{W_{[34]} - W_{[12]}}{Q_{[23]}}$$



# Mechanical components in Rankine Steam Cycle



Steam turbine images removed due to copyright restrictions.

Please see:

<http://nlcs.k12.in.us/oljrhi/brown/power/images/steamturbine.jpg>

## Important design considerations and a more realistic Rankine Cycle

### ★ I Pumps

Real pumps are single phase devices, for pressurizing liquids.

Much easier to pressurize a liquid than a gas

So ① **must be moved to saturation**

Forces massive condensation systems

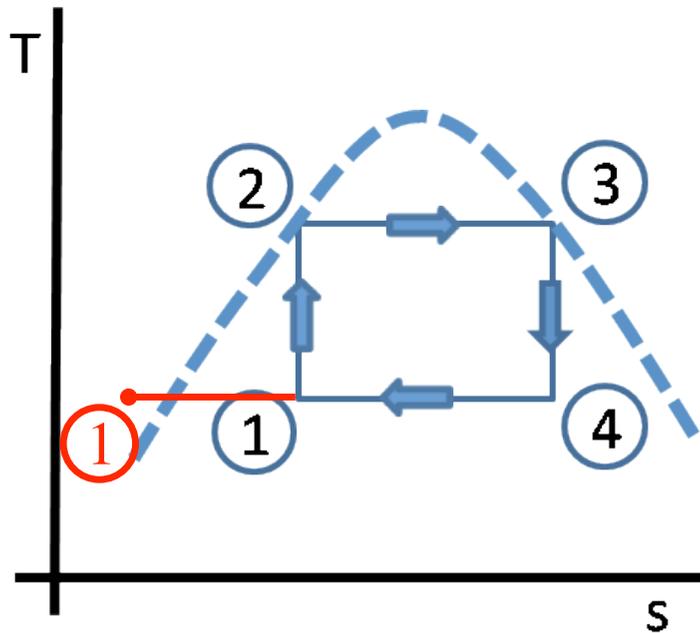


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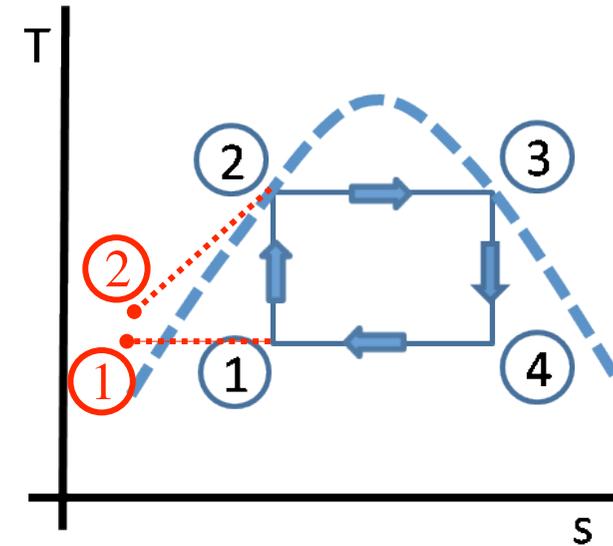
## Important design considerations and a more realistic Rankine Cycle

### ★ II Pumps

Pumps do little work on a liquid ( $dW = p dV$ )

So they do not increase the temperature much

So ② must be moved to lower temperature



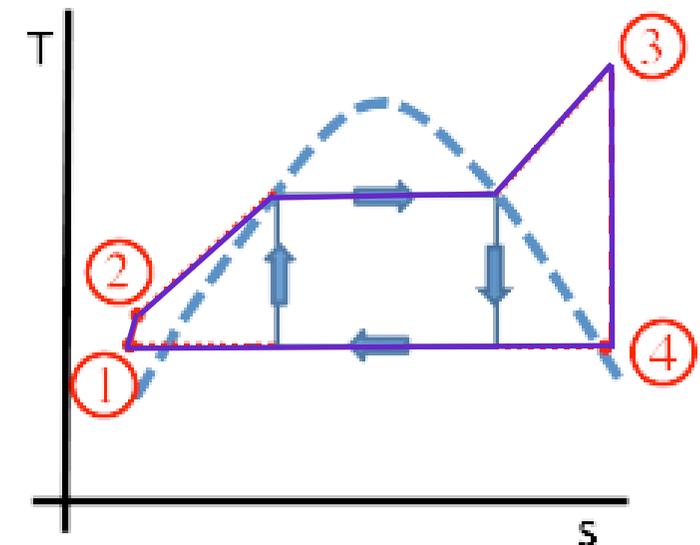
### ★ III Turbines

High performance turbines cannot tolerate a mixed phase

Droplets of liquid damage rotors and quickly degrade performance

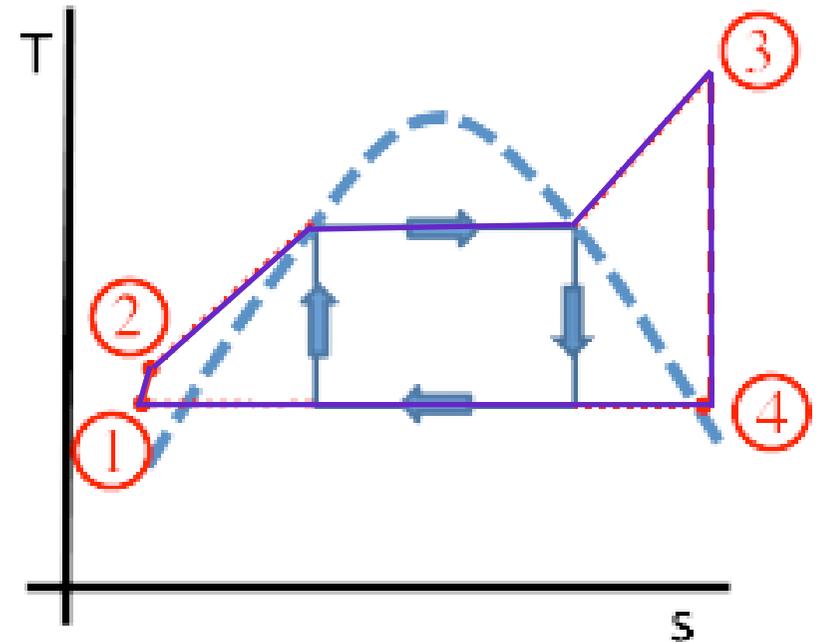
Vapor input to turbine must be superheated

And fluid at outlet must be  $\gtrsim 99\%$  vapor



## Realistic Rankine Cycle and its (less than optimal) consequences!

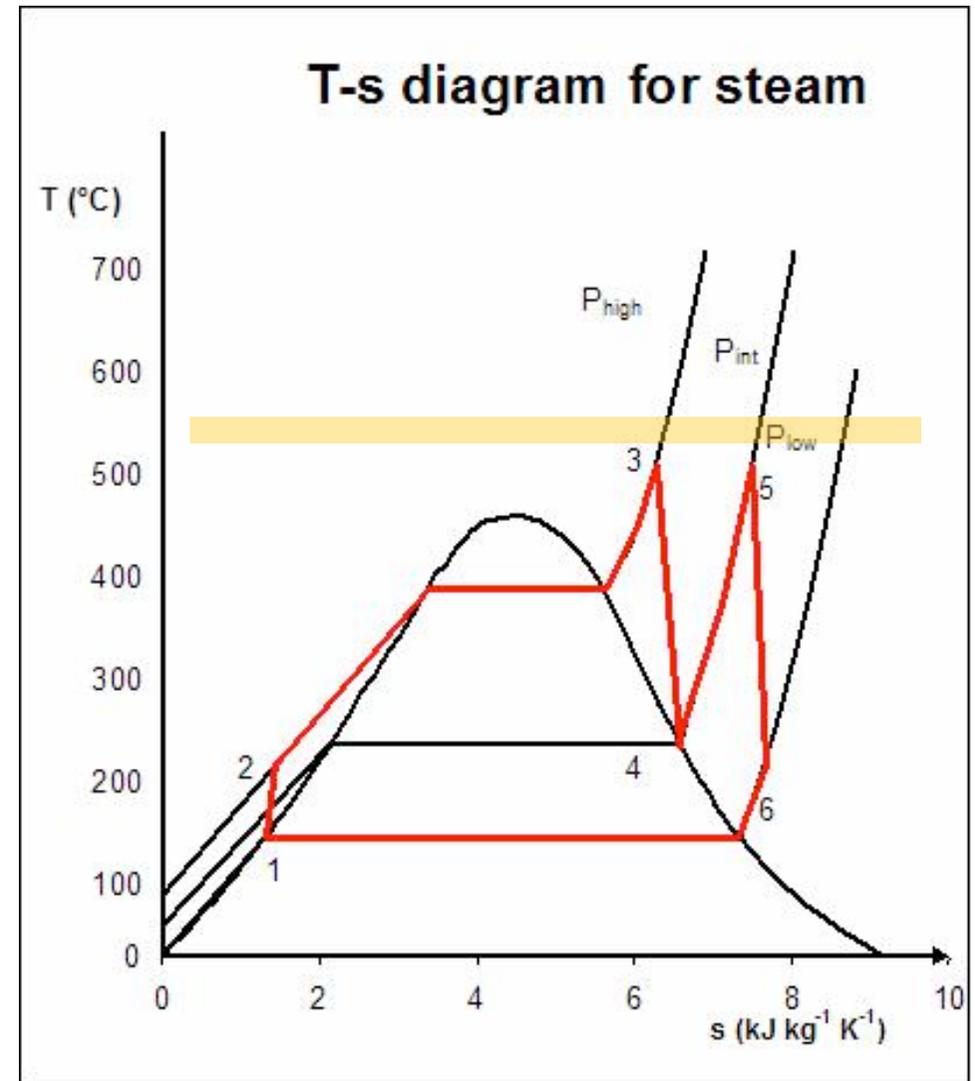
- ★ Latent heat of condensation is not used to power turbine.
- ★ Fluid at output of turbine is saturated, or even superheated, steam, with considerable untapped energy content
- ★ Which must be converted to liquid before it can be cycled through pumps
- ★ Either
  - Waste all that energy up the cooling tower
  - Use it for space heating: **cogeneration!**  
That is: Use the steam for space heating!



# Rankine Cycle with Reheating

## Improving the Rankine Cycle

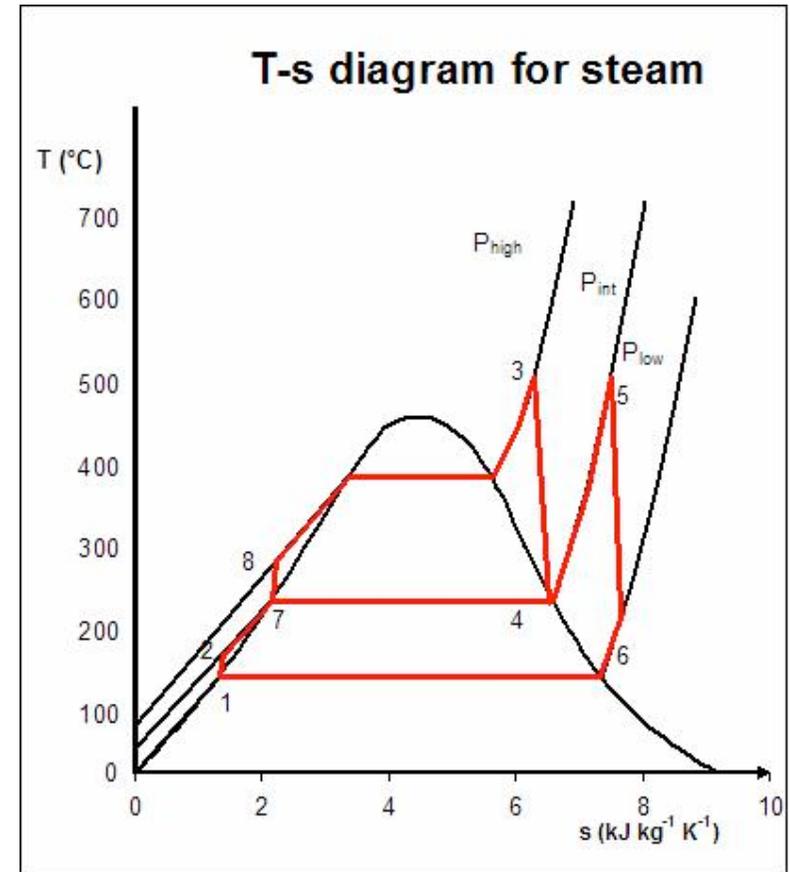
- ★ Use higher temperature and pressure
- ★ Must keep turbine out of mixed phase
- ★ Must not let  $T_H$  exceed  $\sim 550 - 600^\circ\text{C}$
- ★ **Solution: Two turbines with reheating!**



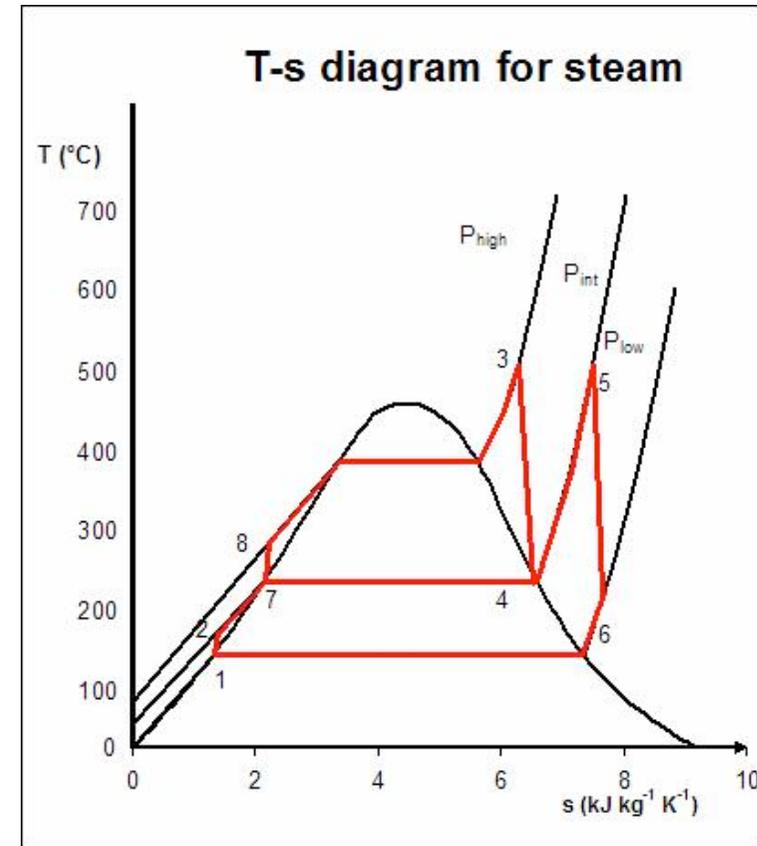
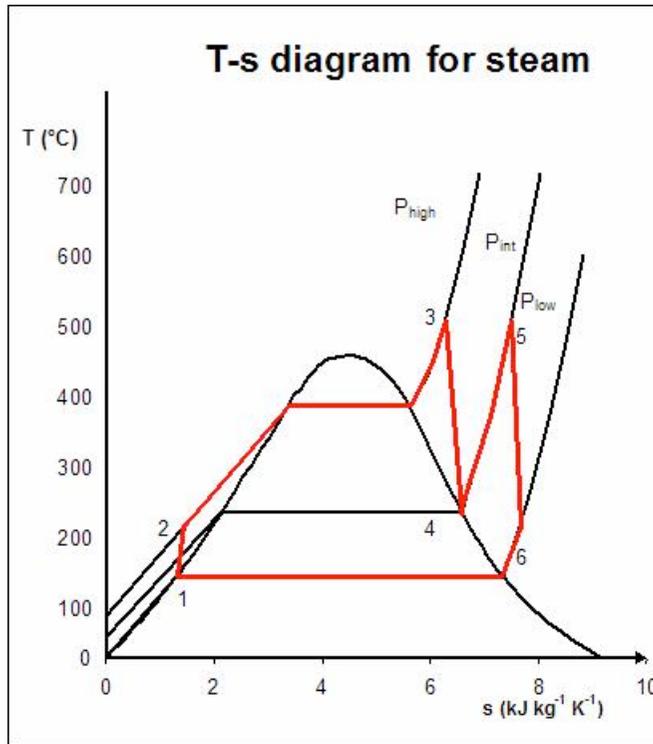
# Rankine Cycle with Regeneration

## Rankine with regeneration:

- Commonly used in actual power plants
- Two turbines in series
- Condensed subcooled liquid at ②
- Mixed with steam tapped at ④
- To preheat to saturated liquid at ⑦



## More complex Rankine cycles



### Rankine with reheat:

- Two turbines in series
- Output from one at ④
- Re-enters boiler without recompression
- Hence no decrease in entropy before reheating
- And then to second turbine

### Rankine with regeneration:

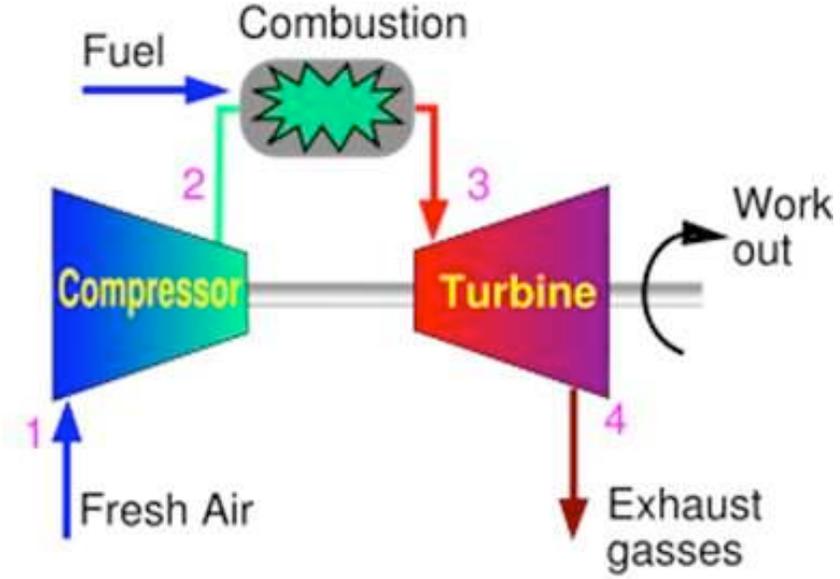
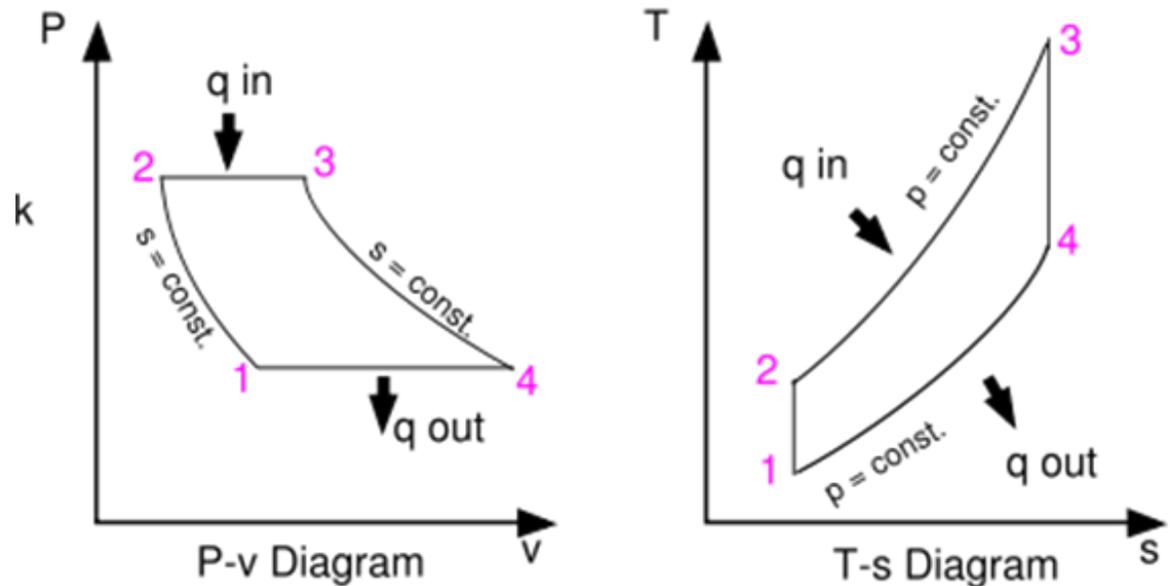
- Commonly used in actual power plants
- Two turbines in series
- Condensed subcooled liquid at ②
- Mixed with steam tapped at ④
- To preheat to saturated liquid at ⑦

# Brayton-Rankine combined cycles

# Brayton Gas Turbine Cycles

## Open cycle gas fired turbine

- ★ What's the idea? Burn natural gas to produce high  $T$  and high  $P$  vapor
- Directly powers turbine
- ★ Very high temperatures  $\sim 1200^{\circ}\text{C}$  and efficiencies  $\sim 35 - 42\%$ .



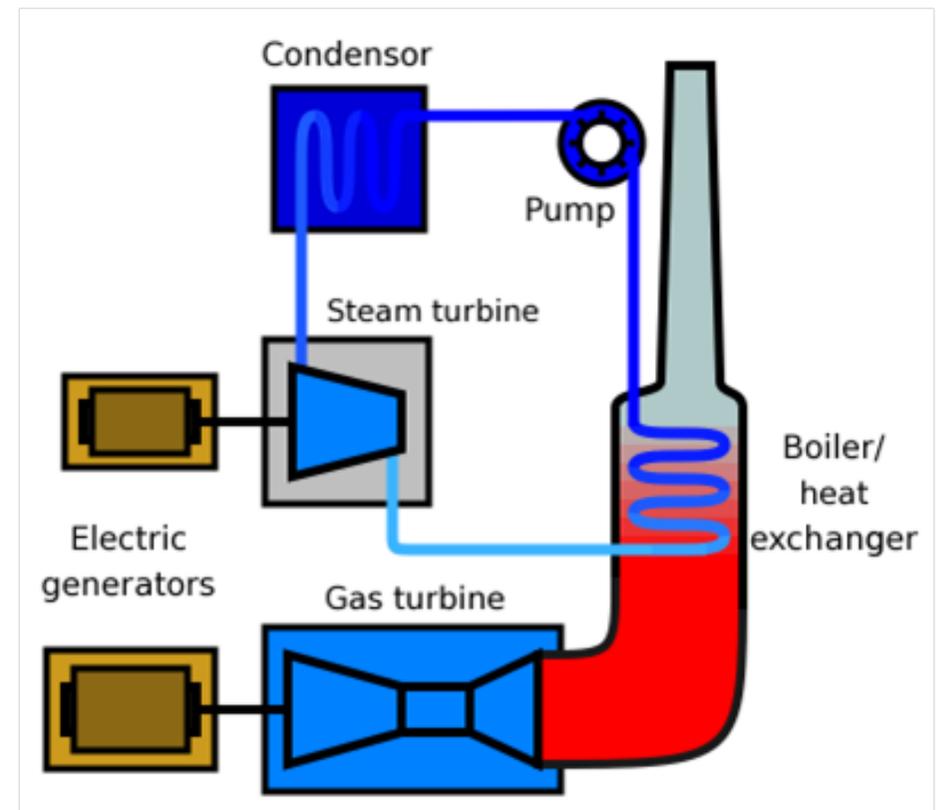
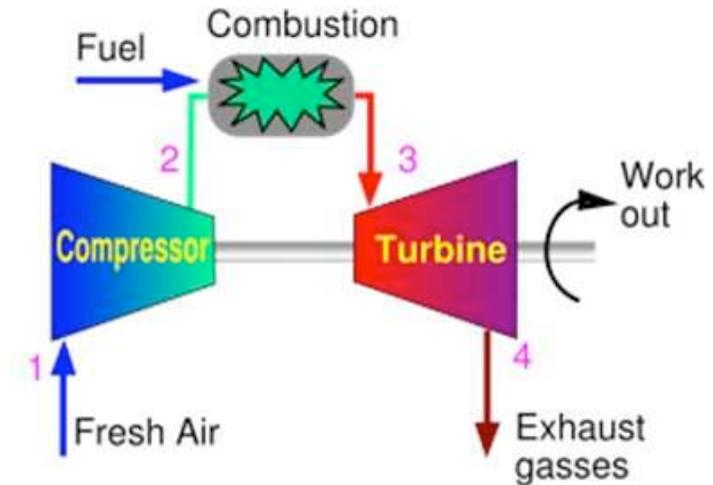
### ★ Elements in cycle

- [12] Fresh air enters compressor: **Adiabatic compression**
- [23] Combustion: **Isobaric heating**
- [34] Turbine: **Adiabatic expansion**
- [41] Exhaust: **Isobaric cooling**

## Brayton Gas Turbine Cycles

### Combine Brayton Gas Cycle with Rankine Steam Cycle

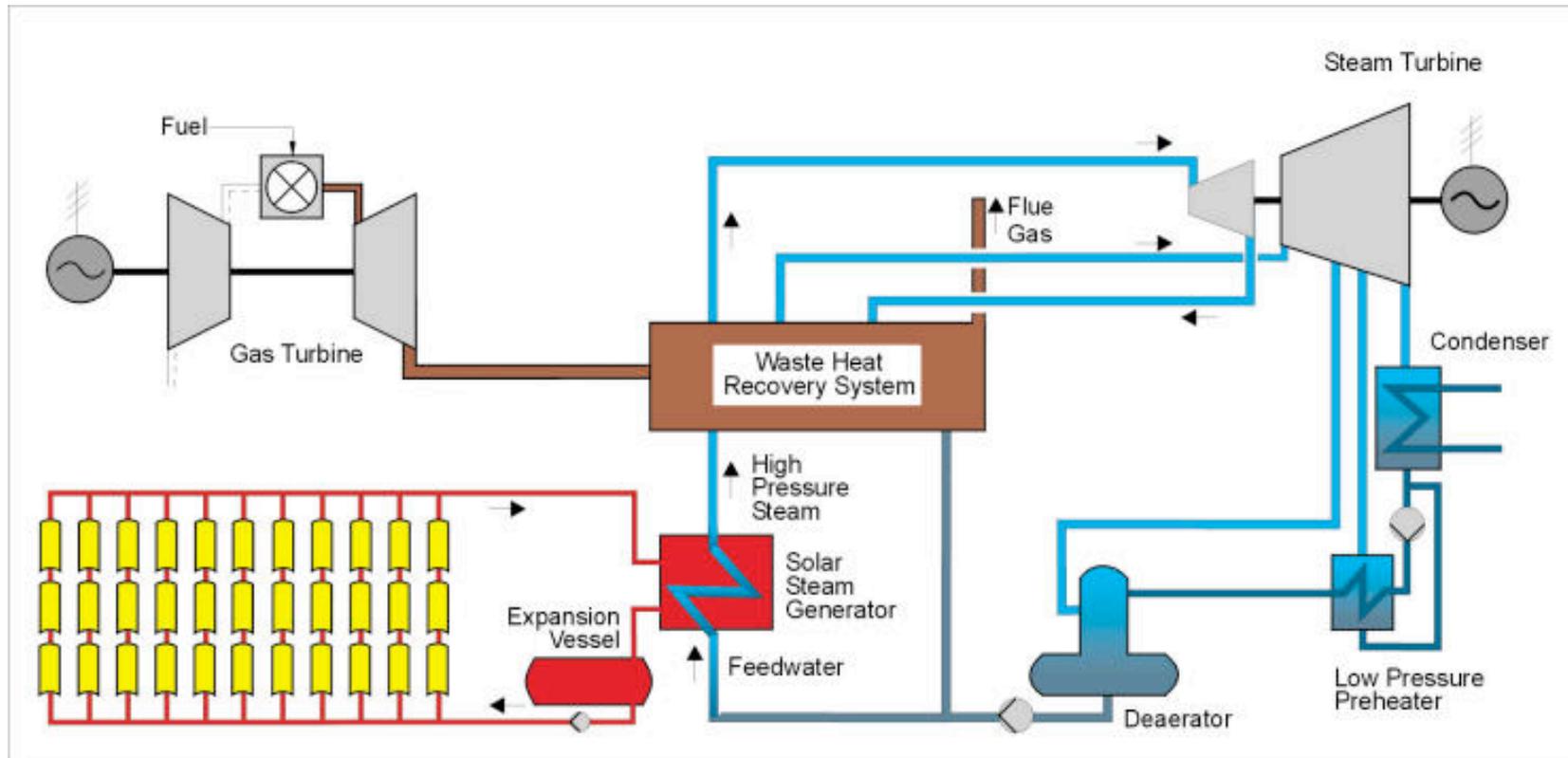
- ★ Very high temperatures  
~ 1200°C and efficiencies  
~ 35 – 42%.
- ★ By-product gases from gas turbine are hot enough,  
~ 500°C to source a downstream Rankine cycle
- ★ Ideally combine with cogeneration for most greatest efficiency!
- ★ Efficiencies exceed **60 – 65 %** compared to 30-40 % for separate Rankine or Brayton cycles (when using natural gas)



# Gas Turbine Combined Cycles

## Combine Brayton Gas Cycle with Rankine Steam Cycle

- ★ Ideally run with natural gas
- ★ Can use syngas from coal gasification. But larger carbon footprint
- ★ Other ideas include integrated solar combined cycle



## Rankine cycles in other applications

★ **Solar thermal energy conversion**

Solar thermal energy conversion image removed due to copyright restrictions.

★ **Ocean thermal energy conversion**

**Using ammonia or other fluid with appropriate thermodynamics**

★ **Low temperature organic Rankine cycles (ORC)**

Please see:

<http://www.inhabitat.com/wp-content/uploads/solarsalt1.jpg>

**Utilize low energy density sources like**

**Biomass, low intensity solar, low temperature geothermal**

**Using organic fluids (eg. pentane) with appropriate thermodynamics**

Image removed due to copyright restrictions.

Please see:

[http://www.evworld.com/images/otec\\_vholstein.jpg](http://www.evworld.com/images/otec_vholstein.jpg)